

FINITE-DIFFERENCE MODEL OF TWO-DIMENSIONAL, SINGLE-, AND TWO-PHASE HEAT TRANSPORT IN A POROUS MEDIUM—VERSION I

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CONTENTS

	Page
Abstract	1
Introduction	2
Model Description	
Theoretical Development	3
Final Equations	4
Auxillary Relationships	5
Numerical Development	13
Finite-difference Representation	15
Solution Procedure	18
Heat Loss Calculations	23
Model Documentation	
Notes on Use of Program	26
Description of the Subroutines	29
Input	33
Output	37
Applications	
Example 1	39
Example 2	44
Notation	50
References	52
Program Listing	54

FIGURES

	Page
1. Pressure-enthalpy diagram for pure water and vapor showing three thermodynamic regions below the critical point: 1) compressed water, 2) two-phase steam and water and 3) superheated steam (modified from White, Muffler, and Truesdell, 1971)	9
2. Finite-difference grid showing the locations of the reservoir, the grid blocks and nodes	14
3. Normal storage of matrix and banded storage of matrix	22
4. Program subroutines showing order and link calling	30
5. Generalized flow chart	32
6. Finite-difference solution for the Avdonin linear example at time = 3.75×10^8 sec; analytical solution indicated by solid line	43
7. Formated Data for Example 2	46
8. Computed pressure distribution at various times for example 2. (After Faust and Mercer, 1976.)	48
9. Computed water saturation distribution for example 2 after 5 years of exploitation. (Single-phase water indicated by shading; solid line: Galerkin finite-element solution; dashed line: finite-difference solution.) After Faust and Mercer, 1976	48

TABLES

	Page
1. Data for Avdonin Linear Example	42
2. Data for Example with Conversion	45

Finite-Difference Model of Two-Dimensional,
Single-, and Two-Phase Heat Transport
in a Porous Medium——Version I

by

Charles R. Faust and James W. Mercer

ABSTRACT

Model documentation is presented for a two-dimensional (areal) heat-transport model capable of simulating both water- and vapor-dominated geothermal reservoirs that conform with the assumptions of the model. Finite-difference techniques are used to solve for the dependent variables pressure and enthalpy. The program is designed to simulate time-dependent problems such as those associated with geothermal reservoirs undergoing exploitation, and can treat the transition from compressed water to two-phase flow. In order to simulate more complicated field problems the present program is being extended, and therefore the model described in this report is referred to as VERSION I. A listing of the computer code is included.

INTRODUCTION

The continuity equations for steam and water are reduced to two nonlinear partial differential equations in which the dependent variables are fluid pressure and enthalpy. These equations are approximated using finite-difference techniques and are solved using a direct matrix technique. The nonlinear coefficients are calculated using Newton-Raphson iteration on the accumulation terms, and an option is provided for using either upstream or midpoint weighting on the mobility terms. The model can simulate flow of compressed water, two-phase mixtures, and super-heated steam over a temperature range of 10° to 300°C. In addition, it can handle the conversion from single-phase flow to two-phase flow.

The model described in this report is referred to as VERSION I and is considered to be a research tool; that is, this version is kept as simple as possible so that the program can be easily understood and modified. For this reason, many sophisticated changes and additions which are generally required to simulate complicated field problems are not included. Such changes are the subject of current research and will be described in subsequent reports.

MODEL DESCRIPTION

Theoretical Development

The computer program presented in this report is based on a theoretical development originally outlined by Mercer, Faust, and Pinder (1974) and presented in detail by Faust (1976). Only the final equations and major assumptions are given here.

Major assumptions include the following:

- 1) capillary pressure is negligible;
- 2) local thermal equilibrium exists among all phases;
- 3) Darcy's equations for two-phase flow are valid;
- 4) the thermodynamic properties of the geothermal fluid are those of a pure-water system;
- 5) thermal dispersion/conduction is treated as a property of the medium;
- 6) flow in the reservoir can be represented by using a two-dimensional (areal) model; and
- 7) the reservoir is a confined porous medium.

Final Equations

Based on these assumptions the equations describing flow and heat transport in a geothermal reservoir are (Faust, 1976):

$$\nabla \cdot \left(\frac{b \rho_s k k_{rs}}{\mu_s} \nabla p \right) + \nabla \cdot \left(\frac{b \rho_w k k_{rw}}{\mu_w} \nabla p \right) + b q'_s + b q'_w = b \frac{\partial(\phi \rho)}{\partial t} \quad (1)$$

and

$$\nabla \cdot \left(\frac{b \rho_s h k k_{rs}}{\mu_s} \nabla p \right) + \nabla \cdot \left(\frac{b \rho_w h k k_{rw}}{\mu_w} \nabla p \right) + \nabla \cdot \{ K_m b [\left(\frac{\partial T}{\partial p} \right)_h \nabla p + \left(\frac{\partial T}{\partial h} \right)_p \nabla h] \} \quad (2)$$

$$+ b q'_s h'_s + b q'_w h'_w + q'' = b \frac{\partial}{\partial t} [\phi \rho h + (1-\phi) \rho_r h_r]$$

where the term, q'' , represents the conductive-heat gain (or loss) to the confining beds (overburden and underburden), and may be obtained from,

$$q'' = K \frac{\partial T}{r \partial z} \Big|_{\text{overburden contact}} - K \frac{\partial T}{r \partial z} \Big|_{\text{underburden contact}} \quad (3)$$

Definitions of the parameters are included in the section on notation.

Auxiliary Relationships

Additional assumptions and relationships include the following:

1) The fluid enthalpy, h , of the mixture is defined in the two-phase region by:

$$h = \frac{S_s \rho_s h_s + S_w \rho_w h_w}{\rho} . \quad (4)$$

2) The density, ρ , of the mixture is defined by

$$\rho = S_s \rho_s + S_w \rho_w . \quad (5)$$

3) Phase saturations sum to one:

$$S_s + S_w = 1 . \quad (6)$$

4) Porosity is a function of pressure, and can be expanded about an initial porosity distribution by a truncated Taylor series with first order pressure terms:

$$\phi = \phi_i [1 + \beta(p - p_i)] , \quad (7)$$

where the subscript i indicates initial values.

5) Phase viscosities are functions of temperature (Meyer and others, 1967; modified for the cgs system),

$$\mu_s = 10^{-6} (0.407 \cdot T + 80.4) , \quad (8)$$

and,

$$\mu_w = 10^{-6} \left\{ 241.4 \cdot 10^{[247.8/(T+133.15)]} \right\}, \quad (9)$$

where,

μ_s = dynamic viscosity of steam, g/cm-sec,

μ_w = dynamic viscosity of water, g/cm-sec,

T = temperature, °C.

Equation 8 is valid for superheated steam at 10^6 dynes per square centimeter pressure in the temperature range of 100 to 300 degrees Celsius, and is approximately valid for steam viscosity along the saturation line in that range. Equation 9 is valid for liquid water along the saturation line from 0 to 300 degrees Celsius.

6) The relative permeability expressions are functions of saturation and are a variation of those given by Corey (1954) for a drainage displacement process, that is, vaporization dominates condensation:

$$k_{rw} = \frac{(S_w - S_{wr} - S_{sr})^4}{(1 - S_{wr} - S_{sr})^4}, \quad (10)$$

and

$$k_{rs} = \left[1 - \frac{(S_w - S_{wr} - S_{sr})}{(1 - S_{wr} - S_{sr})} \right]^2 \cdot \left[1 - \frac{(S_w - S_{wr} - S_{sr})^2}{(1 - S_{wr} - S_{sr})^2} \right], \quad (11)$$

where S_{wr} and S_{sr} are specified residual water and steam saturations.

7) Reservoir thickness, rock density, rock specific heat and intrinsic permeability are functions of the spatial coordinates.

8) Rock enthalpy may be determined by the expression,

$$h_r = c_r T \quad (12)$$

where the rock enthalpy is in ergs per gram, the temperature is in degrees Celsius, and the formation heat capacity, c_r , is in ergs per gram per degree Celsius.

9) In the two-phase region, the amount of heat lost to the well is defined as

$$q_h = q'_s h'_s + q'_w h'_w, \quad (13)$$

and the total mass lost to the well as,

$$q_m = q'_s + q'_w. \quad (14)$$

The steam production rate is determined by the fractional flow of the steam phase as follows,

$$q'_s = \sigma_s q_m, \quad (15)$$

where

$$\sigma_s = k_{rs} / (k_{rs} + \frac{\rho_w u_s}{\rho_s u_w} k_{rw}).$$

Since h'_s , h'_w and q_m are known, q'_s is computed using equation 15, q'_w is computed using equation 14, and q_h is computed using equation 13. Finally, equations relating the thermodynamic properties of pure water and steam to enthalpy and pressure were determined by least square regressions of published experimental data. Figure 1 shows a pressure-enthalpy plot for pure water, this diagram may be divided into the subregions: compressed water, two-phase (steam-water), and superheated steam. Data were obtained from Meyer and others (1967) and Keenan and others (1969) for an enthalpy range of 2.09×10^9 to 3.175×10^{10} ergs per gram, a pressure range of 1.0×10^6 to 1.75×10^8 dynes per square centimeter, and a temperature range of 10 to 300 degrees Celsius. The following expressions, having a maximum error of 0.5 percent within the observed data range, were determined:

10) Steam enthalpy, h_s , and water enthalpy, h_w , are treated as functions of pressure:

$$\begin{aligned} h_s = & 2.82282 \cdot 10^{10} - 3.91952 \cdot 10^{15}/p \\ & + 2.54342 \cdot 10^{21}/p^2 - 9.38879 \cdot 10^{-8} \cdot p^2 \end{aligned} \quad (16)$$

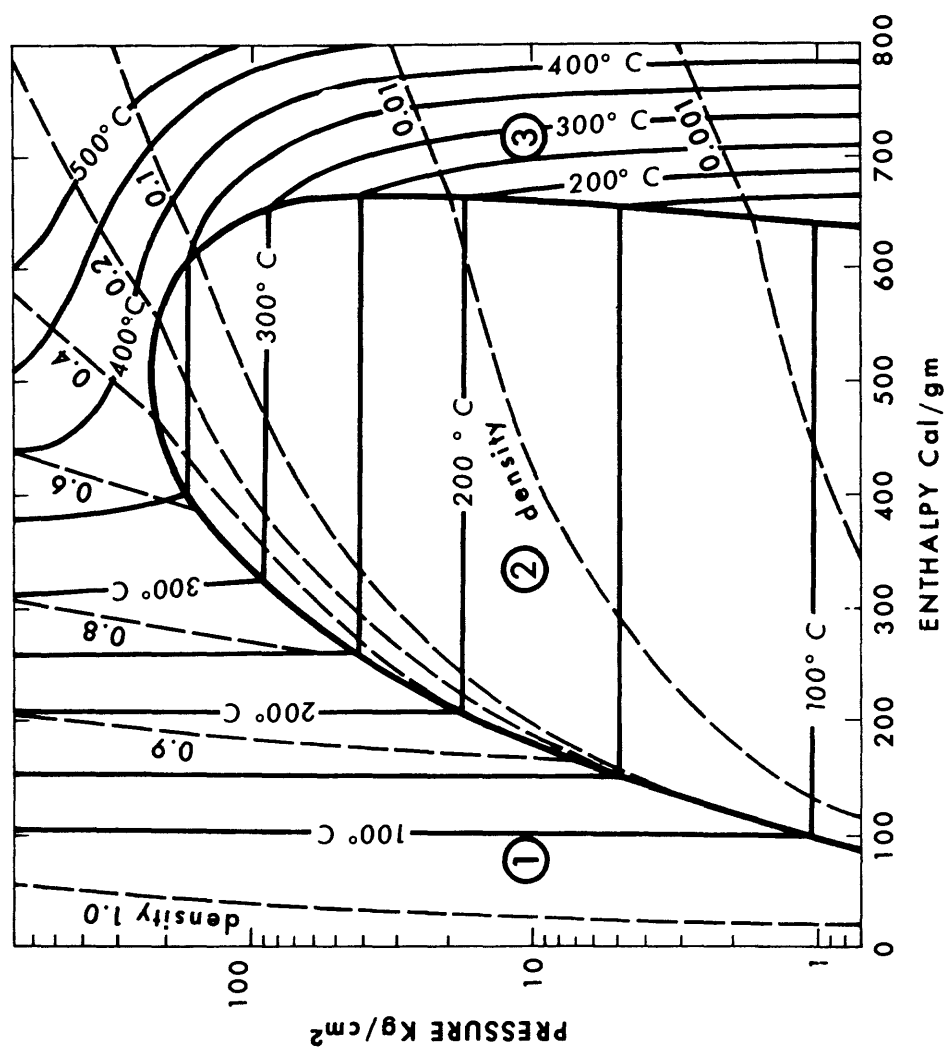


Figure 1. Pressure-enthalpy diagram for pure water and vapor showing three thermodynamic regions below the critical point: 1) compressed water, 2) two-phase steam and water and 3) superheated steam (modified from White, Muffler, and Truesdell, 1971).

and

$$\begin{aligned} h_w = & 7.30984 \cdot 10^9 + 1.29239 \cdot 10^2 p - 1.00333 \\ & 10^{-6} \cdot p^2 + 3.9881 \cdot 10^{-15} \cdot p^3 \\ & - 9.90697 \cdot 10^{15}/p + 1.29267 \cdot 10^{22}/p^2 \\ & - 6.28359 \cdot 10^{27}/p^3, \end{aligned} \quad (17)$$

where

p = pressure, dynes/cm²

h = enthalpy, ergs/g

h_s = enthalpy of saturated steam, ergs/g

h_w = enthalpy of saturated water, ergs/g.

11) Temperature is treated as a function of pressure and enthalpy for the compressed-water and superheated-steam regions. For the compressed-water region,

$$\begin{aligned} T = & - 2.41231 + 2.56222 \cdot 10^{-8} \cdot h \\ & - 9.31415 \cdot 10^{-17} \cdot p^2 \\ & - 2.2568 \cdot 10^{-19} \cdot h^2, \end{aligned} \quad (18)$$

and for the superheated-steam region,

$$\begin{aligned}
 T = & - 374.669 + 4.79921 \cdot 10^{-6} \cdot p \\
 & - 6.33606 \cdot 10^{-15} \cdot p^2 \\
 & + 7.39386 \cdot 10^{-19} \cdot h^2 \\
 & - 3.3372 \cdot 10^{34}/h^2 p^2 \\
 & + 3.57154 \cdot 10^{19}/p^3 \\
 & - 1.1725 \cdot 10^{-37} \cdot h^3 p \\
 & - 2.26861 \cdot 10^{43}/h^4,
 \end{aligned} \tag{19}$$

where the temperature, T , is in degrees Celsius. For the two-phase (steam-water) region h_w is used in place of h in equation 18.

12) Total density, ρ , steam and water densities, ρ_s and ρ_w are considered functions of pressure and enthalpy. For the compressed-water region,

$$\begin{aligned}
 \rho = \rho_w = & 1.00207 + 4.42607 \cdot 10^{-11} \cdot p \\
 & - 5.47456 \cdot 10^{-12} \cdot h \\
 & + 5.02875 \cdot 10^{-21} \cdot hp \\
 & - 1.24791 \cdot 10^{-21} \cdot h^2,
 \end{aligned} \tag{20}$$

and for the superheated-steam region,

$$\begin{aligned}\rho = \rho_s = & - 2.26162 \cdot 10^{-5} + 4.38441 \cdot 10^{-9} \cdot p \\ & - 1.79088 \cdot 10^{-19} \cdot ph \\ & + 3.69276 \cdot 10^{-36} \cdot p^4 \\ & + 5.17644 \cdot 10^{-41} \cdot ph^3 ,\end{aligned}\tag{21}$$

where density is in grams per cubic centimeter. For the steam-water region, saturation pressures and enthalpies are used in equation 20 and 21 to obtain ρ_s and ρ_w .

Numerical Development

The technique used to solve equations 1 and 2 is based on the finite-difference method. For this method the areal extent of the reservoir is subdivided into rectangular grid blocks (see figure 2) in which the fluid and reservoir properties are assumed uniform. The continuous derivatives in equations 1 and 2 are approximated by finite-difference expressions at points (nodes) in the centers of the blocks. This results in a nonlinear system of $2n$ equations with $2n$ unknowns (the values of pressure and enthalpy at the nodes) where n is the number of nodes. The general finite-difference representation and solution procedure for this system of nonlinear equations are outlined below.

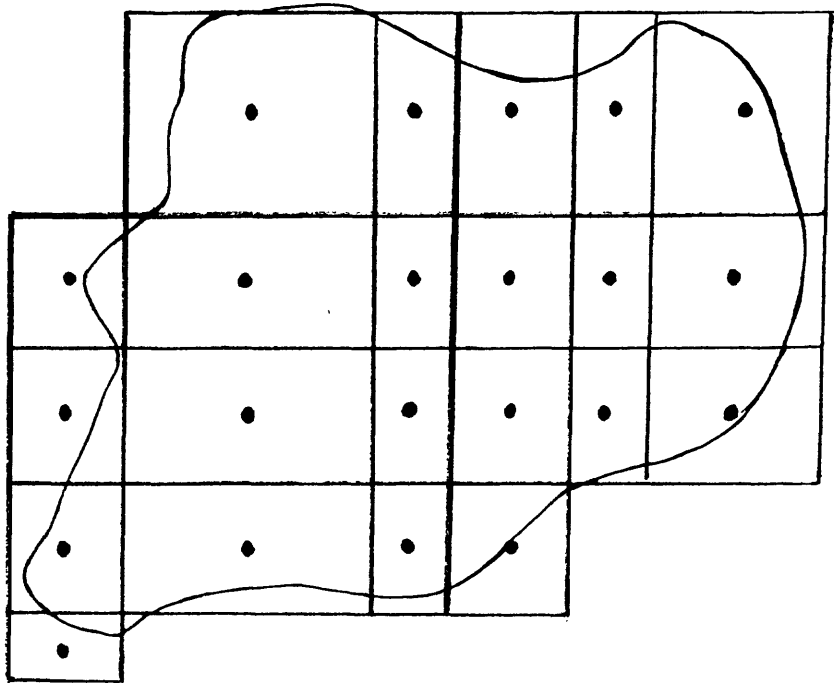


Figure 2. Finite-difference grid showing the locations of the reservoir, the grid blocks and nodes.

Finite-Difference Representation

Equations 1 and 2 may be written in compact, implicit finite-difference form as:

$$\begin{aligned} & \Delta_x [(T_{wx} + T_{sx}) \Delta_x p^{n+1}] + \Delta_y [(T_{wy} + T_{sy}) \Delta_y p^{n+1}] \\ & + V q'_m = \frac{1}{\Delta t} (M^{n+1} - M^n) , \end{aligned} \quad (22)$$

and

$$\begin{aligned} & \Delta_x (T_{hx} \Delta_x p^{n+1}) + \Delta_y (T_{hy} \Delta_y p^{n+1}) + \Delta_x (T_{cx} \Delta_x h^{n+1}) \\ & + \Delta_y (T_{cy} \Delta_y h^{n+1}) + V q'_h + \frac{V}{b} q'' = \frac{1}{\Delta t} (E^{n+1} - E^n) , \end{aligned} \quad (23)$$

where the right sides of equations 22 and 23 are the accumulation terms for mass and energy, respectively, and q'_m and q'_h are the total mass and heat lost to wells, respectively.

The transmissibility terms T_w , T_s , T_h , and T_c , are given by:

$$T_w = (kA/\ell) \rho_w k_{rw} / \mu_w , \quad (24a)$$

$$T_s = (kA/\ell) \rho_s k_{rs} / \mu_s , \quad (24b)$$

$$T_h = T_w h_w + T_s h_s + (AK_m/\ell) \left(\frac{\partial T}{\partial p} \right)_h , \quad (24c)$$

$$T_c = (AK_m/\ell) \left(\frac{\partial T}{\partial h} \right)_p , \quad (24d)$$

and the mass and energy terms M and E are:

$$M = V\phi\rho , \quad (25a)$$

$$E = V[\phi\rho h + (1-\phi)\rho_r h_r] , \quad (25b)$$

where V , A and ℓ are the grid block volume, cross-sectional area perpendicular to the flow direction, and the length increment in the flow direction, respectively. The difference operator acts as follows:

$$\begin{aligned} \Delta_x (T_{wx} \Delta_x p^{t+\Delta t}) &= T_{wx_{i+1/2,j}} (p_{i+1,j}^{t+\Delta t} - p_{i,j}^{t+\Delta t}) \\ &\quad - T_{wx_{i-1/2,j}} (p_{i,j}^{t+\Delta t} - p_{i-1,j}^{t+\Delta t}) , \end{aligned} \quad (26)$$

where i and j are indices in the x - and y - directions, and t is the index for the time level.

The interblock transmissibility terms (values at $i + \frac{1}{2}$, $i - \frac{1}{2}$, $j + \frac{1}{2}$ and $j - \frac{1}{2}$) are composed of two parts: that which is a function of space only (for example, kA/ℓ) and that which is a nonlinear function of pressure and/or enthalpy (for example $\rho k_r/\mu$). To approximate these terms requires averaging or weighting of the various components over each grid block. For the space dependent part, this is accomplished by using a harmonic mean, for example,

$$(kA/\ell)_{i+\frac{1}{2}} = \frac{2k_{i+1}k_i A_{i+1}A_i}{k_{i+1}A_{i+1}\ell_i + k_i A_i \ell_{i+1}} \quad (27)$$

The nonlinear part of the transmissibility terms are generally assigned the upstream value. The upstream node is determined by comparing the pressures at (i) and (i+1), and using the larger pressure to compute the nonlinear part. Alternatively this part may be determined by a length weighted arithmetic average, for example,

$$k_{rw_{i+\frac{1}{2}}} = \frac{k_{rw_{i+1}}\ell_{i+1} + k_{rw_i}\ell_i}{\ell_{i+1} + \ell_i} \quad (28)$$

Of the two procedures, upstream weighting yields a lower order approximation of the spatial derivative but exhibits a more stable solution.

Solution Procedure

The difference equations 22 and 23 are solved simultaneously for the unknown pressure and enthalpy in each grid block for each time step. Since equations 22 and 23 are nonlinear, a provision is included to iterate on nonlinear coefficients. Newton-Raphson iteration is used on the accumulation terms and Picard iteration is used on the coefficients of the spatial derivatives. Two difference equations are obtained for each grid block, and the resulting system of $2n$ equations has the form,

$$[B] \{X^{t+\Delta t}\} - \{f(X^{t+\Delta t})\} + \{f(X^t)\} + \{q\} = 0, \quad (29)$$

where the superscript indicates the time level, the matrix $[B]$ incorporates the transmissibility terms, the vector $\{X\}$ contains the unknown pressure and enthalpy values, that is

$$\{X\} = \begin{Bmatrix} p_1 \\ h_1 \\ p_2 \\ h_2 \\ \vdots \\ p_n \\ h_n \end{Bmatrix}$$

and the vector $\{f(X)\}$ is a non-linear function describing the accumulation terms.

To linearize 29, an iterative technique called the Newton-Raphson procedure is applied. The iteration level is indicated by a subscript, and in particular the first iteration (initial guess) is indicated by the subscript (0). Substitution of the initial guess into equation 29 yields a residual:

$$\begin{aligned} [B_0] \{X_0^{t+\Delta t}\} - \{f(X_0^{t+\Delta t})\} + \{f(X^t)\} \\ + \{q_0\} = \{R(X_0^{t+\Delta t})\} . \end{aligned} \quad (30)$$

For the first time step, the initial conditions are used as the initial guess; for subsequent time steps, the results from the previous time step are used as the initial guess.

If the residual is expanded in a truncated first order Taylor series, one obtains,

$$\{R(X^{t+\Delta t})\} = \{R(X_0^{t+\Delta t})\} + \{\Delta X\} \left[\frac{\partial \{R(X_0^{t+\Delta t})\}}{\partial X_0^{t+\Delta t}} \right] \doteq 0 ,$$

or rearranging,

$$\left[\frac{\partial \{R(X_0^{t+\Delta t})\}}{\partial X_0^{t+\Delta t}} \right] \{\Delta X\} = - \{R(X_0^{t+\Delta t})\} . \quad (31)$$

Taking the derivatives with respect to the unknown vector $\{X\}$ equation 31 yields,

$$\left[\frac{\partial \{R(X_0^{t+\Delta t})\}}{\partial X_0^{t+\Delta t}} \right] = [B_0] - \left[\frac{\partial \{f(X_0^{t+\Delta t})\}}{\partial X_0^{t+\Delta t}} \right] , \quad (32)$$

where $\left[\frac{\partial \{f(X_o^{t+\Delta t})\}}{\partial X_o^{t+\Delta t}} \right]$ is obtained by taking the partial derivatives of the accumulation terms with respect to pressure and enthalpy. Specifically, by use of the chain rule:

$$b \frac{\partial(\phi\rho)}{\partial p} = b \left[\rho \frac{d\phi}{dp} + \left(\frac{\partial\rho}{\partial p} \right)_h \right]$$

$$b \frac{\partial(\phi\rho)}{\partial h} = b \left(\frac{\partial\rho}{\partial h} \right)_p ,$$

$$b \frac{\partial}{\partial p} \left[\phi\rho h + (1-\phi)\rho_r h_r \right] = b \left[(\rho h - \rho_r h_r) \frac{d\phi}{dp} + h \left(\frac{\partial\rho}{\partial p} \right)_h + (1-\phi)\rho_r c_r \left(\frac{\partial T}{\partial p} \right)_h \right] ,$$

and

$$b \frac{\partial}{\partial h} \left[\phi\rho h + (1-\phi)\rho_r h_r \right] = b \left[\phi h \left(\frac{\partial\rho}{\partial h} \right)_p + (1-\phi)\rho_r c_r \left(\frac{\partial T}{\partial h} \right)_p + \phi\rho \right] .$$

Substituting 32 into equation 31 gives,

$$\left[\left[B_o \right] - \left[\frac{\partial \{f(X_o^{t+\Delta t})\}}{\partial X_o^{t+\Delta t}} \right] \right] \{ \Delta X \} = - \{ R(X_o^{t+\Delta t}) \} , \quad (33)$$

which is the matrix equation to be solved.

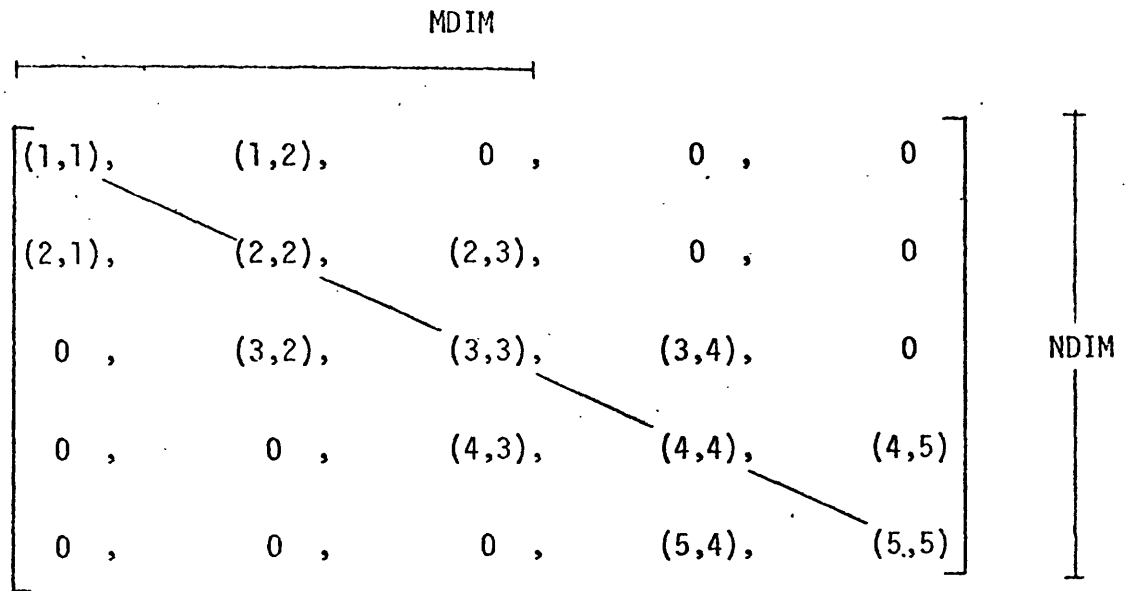
The new values of $X^{t+\Delta t}$ are determined from,

$$\{X_i^{t+\Delta t}\} = \{X_{i-1}^{t+\Delta t}\} + \{\Delta X\} , \quad (34)$$

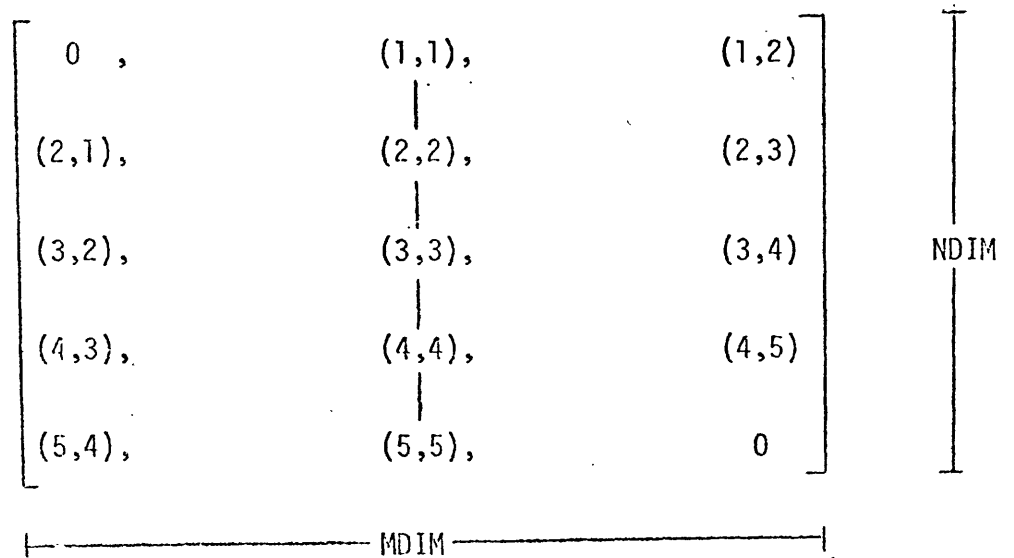
where $i = 1, 2, \dots, m$, m being the specified number of iterations. If $m = 1$, this procedure is equivalent to the residual formulation outlined by Weinstein, Stone, and Kwan (1969).

In most of the two-dimensional, areal simulations studied it was not necessary to use Newton-Raphson iteration on the nonlinear coefficients in $[B]$ and $\{q\}$ to obtain satisfactory solutions. For radial problems and vertical cross-sections this is not the case as pointed out by Toronyi and Farouq Ali (1975). As stated earlier, Picard iteration is used for $[B]$ and $\{q\}$. In this process the nonlinear coefficients are simply updated on each iteration.

The solution of the linearized matrix equation 33 is solved using the Gauss-Doolittle method for banded, nonsymmetric matrices. The coefficient matrix is decomposed into the product of upper and lower triangular matrices, from which the solution may be determined by back substitution. Because the coefficient matrix is nonlinear, this solution procedure is required for each iteration of each time step. The general form of the coefficient matrix and the form in which it is stored in the program is shown in figure 3, where MDIM is the matrix bandwidth and NDIM is the number of rows.



a. Normal storage of matrix where bold marks indicate the main diagonal.



b. Banded storage of matrix showing new location of the main diagonal.

Figure 3. Normal storage of matrix and banded storage of matrix.

Heat Loss Calculations

Geothermal reservoirs occur in areas of anomalously high heat flow. The effects of the high geothermal gradient and the loss and gain of heat to the base and cap rock are important factors that are incorporated into the reservoir model. In a typical hydrothermal system, heat flows into the reservoir at the base and out at the top.

In order to obtain the heat flux through the confining beds three simplifying assumptions are made. First, the permeability in the confining bed is assumed to be low and convective flow may be neglected; thus, only the heat conduction equation needs to be solved. Further, the horizontal conduction terms in the confining beds are assumed to be small relative to the vertical terms, and may be neglected. For petroleum reservoirs undergoing thermal recovery, it has been demonstrated that the effect of horizontal conduction in the confining beds is small (Chase and O'Dell, 1973). This assumption leads to the one-dimensional, heat-conduction equation:

$$K_r \frac{\partial^2 T'}{\partial z^2} = (\rho c)_r \frac{\partial T'}{\partial t} ,$$

where the vertical thermal conductivity, density, and heat capacity of the confining bed are considered constant. The final assumption is that the geothermal reservoir, prior to exploitation, is at steady state; that is, the heat entering at the base equals that leaving at the top and the net heat gain of the reservoir is zero. This assumption allows consideration of only the "transient" heat flow caused by temporal temperature changes in the reservoir.

Therefore, the one-dimensional, conduction equation may be reformulated as follows:

$$K_r \frac{\partial^2 T^*}{\partial z^2} = (\rho c)_r \frac{\partial T^*}{\partial t} , \quad (35)$$

where $T^* = T' - T'_0$ (T' is the temperature in the confining bed and T'_0 is the initial temperature in the confining bed.)

Equation 35 is subject to initial and boundary conditions. The initial conditions are simply $T^*(z,0) = 0$. For the boundary condition at the top of the cap rock, the temperature change is assumed to be zero for all time. At the cap rock-reservoir boundary, a step function in temperature is used. It is determined using the difference between the initial reservoir temperature and the reservoir temperature at the last time step (that is, the step function is lagged by one time step). Once the T^* distribution through the cap rock is determined, Fourier's equation is used to compute the heat flux.

A similar set of boundary and initial conditions apply to the base rock; however, instead of solving equation 35 for both the top and bottom, it is assumed that the two fluxes are approximately equal and therefore the total heat leakage is obtained by multiplying the flux computed at the top by two. This assumption is valid since only the "transient" heat leakage is considered; however, this portion of the program could be modified if needed (for example, if steady state thermal gradients above and below the reservoir are significantly different).

In the numerical model, equation 35 is actually solved at each grid block for each iteration. It is solved using a Galerkin, finite-element approximation for the space derivative combined with an implicit difference approximation for the time derivative. Linear elements are used with a variable mesh generator that divides the confining bed thickness into ten elements that double in size with distance from the reservoir boundary. Therefore, the element adjacent to the reservoir is relatively small, and it is the temperature difference across this element that is used in Fourier's equation to compute the heat flux.

MODEL DOCUMENTATION

Notes on Use of Program

- (1) This version of the finite-difference model is restricted to problems involving confined, horizontal reservoirs exhibiting two-dimensional flow. Furthermore, the reservoir is overlain and underlain by impermeable layers that allow only conduction of heat.
- (2) To minimize core requirements, the dimensions of the arrays A(NBB,MBE) and R(NBB) must be specified for each problem, where

$$NBB = 2 * NB$$

(NB - number of nonzero blocks, that is, blocks that have nonzero permeability) and MBE is the estimated matrix bandwidth given for two simultaneous unknowns at each grid block by

$$MBE = 2 * (2 * MM + 1) + 1$$

where,

$$MM = NY \text{ IF } NX > NY$$

$$MM = NX \text{ IF } NY > NX$$

and NX and NY are the number of columns and rows, respectively.

- (3) The actual matrix bandwidth is computed internally and printed. If it differs from the estimated bandwidth, change MBE so that it is equal to the actual matrix bandwidth. Also, change the dimensions of array A.
- (4) The regression equations used in this program are based on steam table data for a temperature range of 10° to 300°C.
- (5) The units of the input data must be in the cgs system.
- (6) At present most arrays are dimensioned to solve problems with a maximum of 20 columns and 10 rows.

- (7) Relative permeability functions described in equations 10 and 11 are programmed in SUBROUTINE PRPTY statement numbers PRP1230 - PRP1300 where the residual water saturation, $S_{wr} = 0.3$ and the residual steam saturation, $S_{sr} = 0.05$. Other equations may be substituted for these; the only restriction is that relative permeability must be a smooth function of saturation. A non-smooth relationship (such as linear interpolation between data points) can result in an oscillatory, unstable solution.
- (8) The two-dimensional treatment in this model assumes that the fluid properties are uniform with depth. This assumption is probably valid only for very thin reservoirs, but may be a suitable approximation for some applications.
- (9) The program should be in double precision, except when using a computer having single precision accuracy to 10 significant digits, in which case remove the REAL*8 IMPLICIT cards.
- (10) Although the unknown dependent variables are pressure and enthalpy, the user is given the option to read in either initial pressures and temperatures ($K\emptyset D9 = 1$) or initial pressures and enthalpies ($K\emptyset D9 = 0$). This option is provided since field temperatures are more readily available than enthalpies. If temperatures are read, they are converted in the program to enthalpies, and subsequent calculations are made using the enthalpy values. If the initial conditions of the reservoir are two phase, the user must read in enthalpies.

- (11) To reduce the number of lines in the output, only the computed pressures and enthalpies are printed for each time step. The user may, however, also have the computed water saturations, temperatures, and fluid densities printed as often as desired by specifying the proper value for IPRT. This parameter allows the additional data to be printed every IPRT time step. For example, if $IPRT = 10$, saturations, temperatures and densities will be printed on time step 1, 10, 20, . . . until the end of the simulation.
- (12) Minimum number of blocks required for a successful run are two in the x-direction and two in the y-direction.

Description of the Subroutines

The FØRTRAN IV code contains a main program and 12 subroutines, which are shown diagrammatically in Figure 4. The purpose of each subroutine is listed below.

MAIN Driving program for the subroutines. In addition, the large arrays, A and R, are dimensioned to minimize core requirements.

GDATA Reads and writes problem information according to the formats listed in the INPUT section of this report.

READ Reads the two dimensional arrays containing data for each finite-difference block.

TCALC Computes the interblock transmissibility terms. Intrinsic permeability is determined as a harmonic mean of the values in the two blocks.

MATR Computes and prints matrix bandwidth. The estimated bandwidth should equal the computed bandwidth. The bandwidth is used in dimensioning arrays, and if the estimated and computed bandwidths are not equal, computational errors could result. See the section on 'Notes on Use of Program' for details on how to calculate the estimated bandwidth.

PRPTY Computes thermodynamic properties based on regression equations determined using data from steam tables.

VERTCD Computes vertical conductive heat leakage through a confining bed. This is accomplished by solving the one-dimensional, heat-conduction equation at each finite-difference grid block. The numerical method used in this subroutine is the finite-element method.

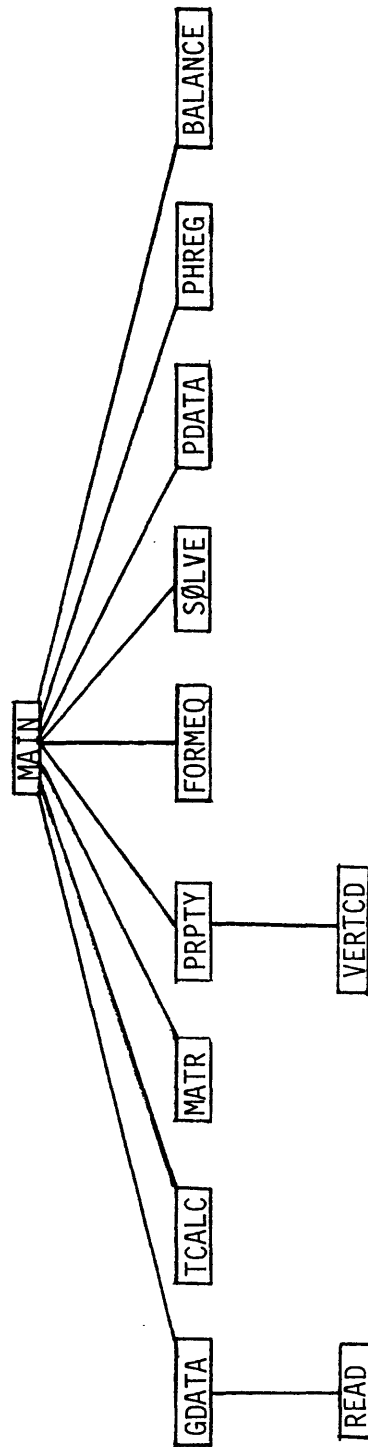


Figure 4. Program subroutines showing order and link of calling.

FØRMEQ Forms the final matrix equation. Note that the matrix is nonsymmetric and that the dependent variables, pressure and enthalpy are solved simultaneously.

SØLVE Solves the matrix equation using the Gauss-Doolittle method. It triangularizes a banded nonsymmetric matrix and then back substitutes.

PDATA Prints the computed pressures and enthalpies for each time step.

PHREG Determines the thermodynamic region for each finite-difference grid block.

BALNCE Computes a mass and energy balance for each time step.

A generalized flow chart showing the approximate order that the subroutines are used is shown in Figure 5.

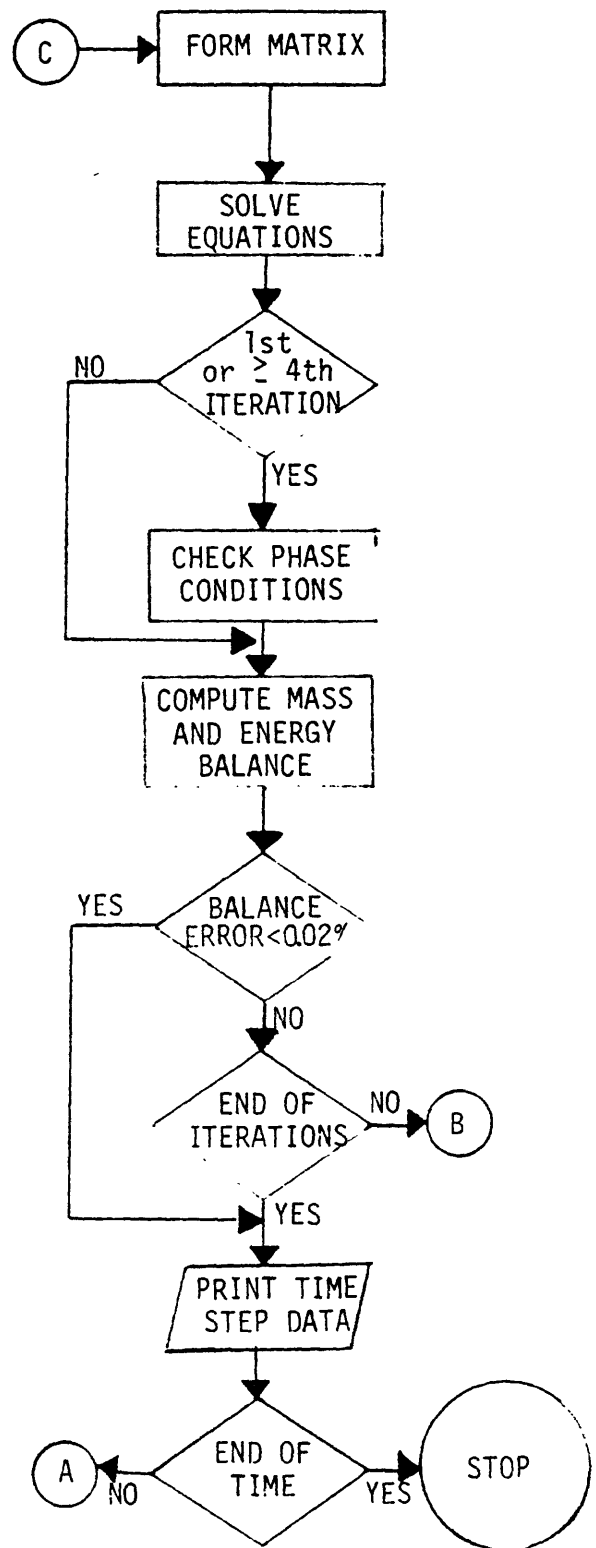
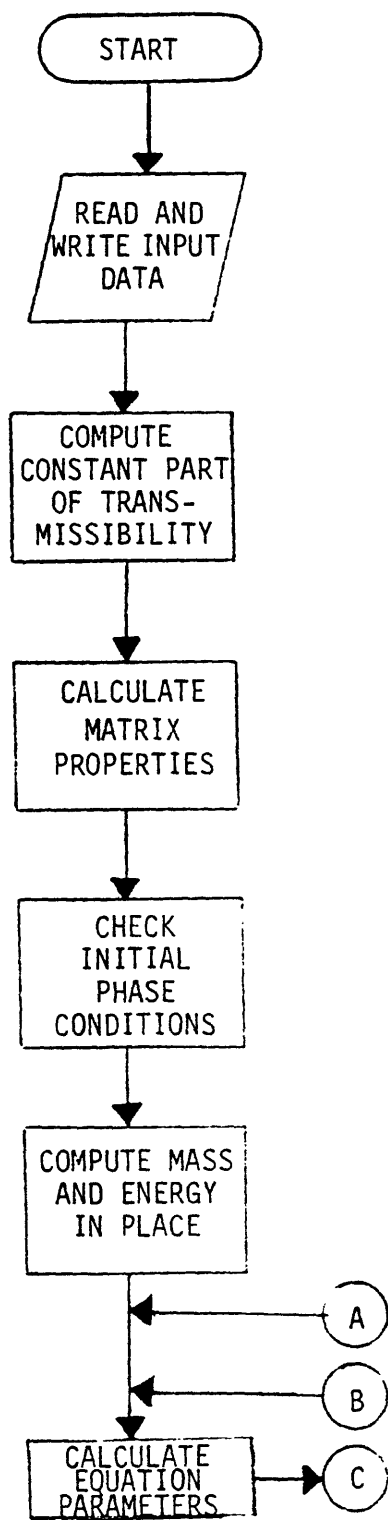


Figure 5. Generalized flow chart.

Input

<u>Columns</u>	<u>Format</u>	<u>Name</u>	<u>Description</u>
<i>Card 1</i>			
1-80	20A4	TITLE	Problem title
<i>Card 2</i>			
1-5	I5	NX	Number of columns (x-direction)
6-10	I5	NY	Number of rows (y-direction)
11-15	I5	NB	Number of non-zero blocks (those with non-zero permeability)
16-20	I5	NK	Maximum number of Newton iterations
21-25	I5	NT	Maximum number of time steps
26-30	I5	NS	Number of sources
31-35	I5	MBE	Estimated bandwidth (see text)
36-40	I5	IØPT	Read 1 for upstream weighting; 2 for midpoint weighting (See section on Finite-Difference Representation)
41-45	I5	PPRT	Number of time steps between printing thermodynamic data
<i>Card 3</i>			
1-10	G10.0	DELT	Time step (in seconds)

<u>Columns</u>	<u>Format</u>	<u>Name</u>	<u>Description</u>
<i>Card 4</i>			
1-5	I5	KØD1	Read 1 if x-spacing is constant (otherwise, leave blank)
6-10	I5	KØD2	Read 1 if y-spacing is constant
11-15	I5	KØD3	Read 1 if initial pressure is constant
16-20	I5	KØD4	Read 1 if initial enthalpy is constant
21-25	I5	KØD5	Read 1 if x-permeability is constant
26-30	I5	KØD6	Read 1 if y-permeability is constant
31-35	I5	KØD7	Read 1 if initial porosity is constant
36-40	I5	KØD8	Read 1 if reservoir thickness is constant
41-45	I5	KØD9	Read 1 if temperature is read in place of enthalpy

Data Set 1 - X-spacing

1-80	8G10.0	DX(I)	Spacing in the x-direction (NX values); if constant, KØD1 = 1 and only read one value (cm)
------	--------	-------	--

Data Set 2 - Y-spacing

1-80	8G10.0	DY(J)	Spacing in the y-direction (NY values); if constant, KØD2 = 1 and only read one value (cm)
------	--------	-------	--

*Data Set 3 - Initial pressure**

1-80	8G10.0	P(I,J)	Initial pressure distribution in the reservoir; if constant, KØD3 = 1 and only read one value (dynes/cm ²)
------	--------	--------	--

*Start new card for the beginning of each new row (may start with the top row or bottom row, but be consistent) leaving blanks for missing blocks.

<u>Columns</u>	<u>Format</u>	<u>Name</u>	<u>Description</u>
<i>Data Set 4 - Initial enthalpy *+</i>			
1-80	8G10.0	H(I,J)	Initial enthalpy distribution in the reservoir; if constant, KØD4 = 1 and only read one value (ergs/g)
<i>Data Set 5 - X-permeability*</i>			
1-80	8G10.0	XK(I,J)	Reservoir permeability in x-direction; if constant, KØD5 = 1 and only read one value (cm ²)
<i>Data Set 6 - Y-permeability*</i>			
1-80	8G10.0	YK(I,J)	Reservoir permeability in y-direction; if constant, KØD6 = 1 and only read one value (cm ²)
<i>Data Set 7 - Porosity*</i>			
1-80	8G10.0	PHI(I,J)	Reservoir porosity; if constant, KØD7 = 1 and only read one value (dimensionless)
<i>Data Set 8 - Thickness*</i>			
1-80	8G10.0	DZ(I,J)	Reservoir thickness; if constant, KØD8 = 1 and only read one value (cm)

* Start new card for the beginning of each new row (may start with the top row or bottom row, but be consistent) leaving blanks for missing blocks.

+ If KØD9 = 1, read initial temperature distribution (°C) instead.

<u>Columns</u>	<u>Format</u>	<u>Name</u>	<u>Description</u>
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Data Set 9 - Sources

1-5	I5	I	Column number of well
6-10	I5	J	Row number of well
11-25	G15.0	Q(I,J)	Strength (g/s) of source/sink at block i,j

Note: 1-NS cards; if NS = 0 this data set is omitted.

Card 5

1-10	G10.0	XKC	Medium thermal conductivity of the reservoir (ergs/s-cm°C)
11-20	G10.0	CØND	Confining bed thermal conductivity (ergs/s-cm°C)
21-30	G10.0	PHFWT	Rock enthalpy derivative with respect to temperature (specific heat) (ergs/g°C)
31-40	G10.0	DF	Rock density (g/cm ³)
41-50	G10.0	BETA	Compressibility of reservoir (cm ² /dyne)

Output

To aid the user in detecting errors associated with data input, data that is read in is immediately printed; thus output appears in the following order:

Title of Problem
Finite-Difference Data
Grid Numbers
Time Parameters
Codes
Spacing in X-Direction
Spacing in Y-Direction
Initial Pressure
Initial Enthalpy
X-Permeability
Y-Permeability
Initial Porosity
Reservoir Thickness
Sources
Rock Properties
Maximum Bandwidth

In addition, every IPRT time step the following is also printed:

Water Saturations
Temperatures
Density



Printed at beginning of time step,
but are based on pressure and enthalpy
from previous time step.

Finally, on a successful run, the following is printed every time step:

Step Number

Time

Pressure Values

Enthalpy Values

Mass and Energy Balance

APPLICATIONS

Example 1

The linear flow of hot incompressible fluid through a confined aquifer may be described by the following equations:

$$K_r \frac{\partial^2 u}{\partial z^2} = \rho_r c_r \frac{\partial u}{\partial t}, \quad z > 0, \quad t > 0 \quad (36a)$$

$$K_t \frac{\partial^2 u}{\partial x^2} - v_w \rho_w c_w \frac{\partial u}{\partial x} + \frac{2}{b} K_r \frac{\partial u}{\partial z} = \rho_t c_t \frac{\partial u}{\partial t}, \quad z = 0, \quad x > 0, \quad t > 0 \quad (36b)$$

subject to:

$$u(x, 0) = 0, \quad x > 0$$

$$u(0, t) = 1, \quad z = 0, \quad t \geq 0$$

$$\text{limit } u = 0$$

$$x^2 + z^2 \rightarrow \infty$$

where $u = \frac{T - T_0}{T_1 - T_0}$ is the normalized temperature; T_0 is the overburden

(underburden) temperature and the initial aquifer temperature; and T_1 is the temperature of the injection fluid. The subscripts refer to the rock, r, water, w, and total (rock and water), t.

Avdonin (1964) presents an analytical solution for equation (36):

$$u(\chi, \tau) = \frac{\chi}{\sqrt{\pi\tau}} \int_0^1 \left\{ \exp \left[- (s\gamma\sqrt{\tau} - \frac{\chi}{2s\sqrt{\tau}})^2 \right] \operatorname{erfc} \left(\frac{qs^2\sqrt{\tau}}{2\sqrt{1-s^2}} \right) \right\} \frac{ds}{s^2} \dots$$

$$\text{where } \chi = \frac{2x}{b}; \quad \tau = \frac{4K_t t}{c_t \rho_t b^2}; \quad \gamma = \frac{Q c_w \rho_w}{4K_t};$$

$$\alpha = \sqrt{\frac{K_x c_x \rho_x}{K_t c_t \rho_t}}; \quad \text{and } Q \text{ is the injection flow rate. (In the}$$

original reference, γ is defined with an 8 in the denominator; this appears to be a typographical error.)

To simulate this problem, the following assumptions were made:

1) Temperature is a function of enthalpy only, according to:

$$T = -0.0208 + 2.39 \times 10^{-8} h \quad (38)$$

2) Density is a function of pressure only, according to:

$$\rho = 0.989875 + 4.00894 \times 10^{11} p \quad (39)$$

3) Porosity is constant.

These changes must be made in the program by appropriately changing the single-phase (water) statement functions for temperature and density, and by appropriately changing their respective pressure- and enthalpy-derivatives. For constant porosity, beta is read as zero. Other parameters and the initial conditions used in this example are given in table 1. A block-centered grid consisting of 20 blocks was used, and the time step was 6.25×10^6 sec. The total simulation time was 3.75×10^8 sec.

The results are presented in figure 6. This problem was chosen because it exhibits pronounced truncation error in the approximation of the spatial derivatives. Time steps were chosen to reduce time truncation errors. Both mid-point weighting and upstream weighting were used. It is clear that mid-point weighting approximates the temperature front better than upstream weighting, but exhibits oscillations at the base of the front. Upstream weighting smears the front out by numerical diffusion and does not exhibit oscillations.

TABLE 1 - DATA FOR AVDONIN LINEAR EXAMPLE

PARAMETER	SYMBOL	VALUE
velocity	v	1.28×10^4 cm/sec
porosity	ϕ	0.20
reservoir thermal conductivity	K_m	3.20×10^6 ergs/sec-cm °C
confining bed thermal conductivity	K'	3.20×10^5 ergs/sec-cm °C
rock density	ρ_r	2.50 g/cm ³
rock specific heat	c_r	1.01×10^7 ergs/g °C
aquifer thickness	b	2.00×10^4 cm
initial pressure	p_i	1.38×10^7 dynes/cm ²
initial enthalpy	h_i	3.35×10^9 ergs/g
initial fluid viscosity	μ_i	3.58×10^{-3} g/cm-sec
initial temperature	T_i	80.19 °C
injection temperature	T'	40.01 °C
fluid density	ρ	0.99 g/cm ³
fluid specific heat	c_w	4.18×10^7 ergs/g °C

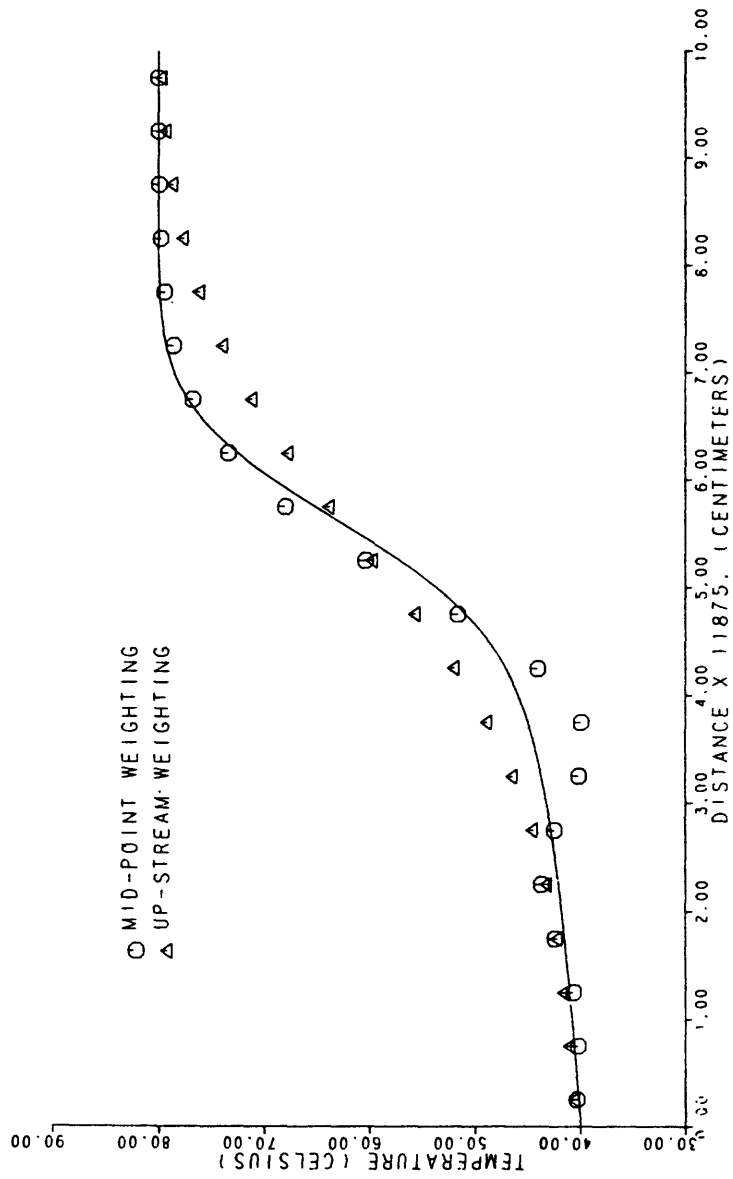


Figure 6. Finite-difference solution for the Avdonin linear example at time = 3.75×10^8 sec; analytical solution indicated by solid line.

Example 2

This example was designed to demonstrate the behavior of an initially hot-water geothermal reservoir that develops a two-phase zone under the influence of production. This problem was originally solved using a finite-element model and a five year simulation period (Faust and Mercer, 1975) and was rerun later under the same conditions using a finite-difference model (Faust and Mercer, 1976). The finite-difference simulation in this report is the same as that presented in the above references, however this simulation stops after 104 days.

Data for this example is given in table 2. This is a one-dimensional problem and therefore only one row is used in conjunction with ten columns, giving ten non-zero blocks. It is assumed that the reservoir is closed to the flow of heat and mass at all boundaries. The time step is 5.0×10^5 seconds and the maximum number of time steps is 18, with a maximum of twelve iterations. The estimated bandwidth is seven, and the spacings in the x- and y-directions are 2.0×10^4 cm and 5.0×10^4 cm respectively. Upstream weighting is used and there is only one sink located (at the left end) in the first block (1,1). A listing of the formatted model data is given in figure 7. Finally, the relative permeabilities used for this problem are:

$$k_{rw} = [(S_w - 0.35)/0.65]^4 \quad (40)$$

and

$$k_{rs} = \{1.0 - [(S_w - 0.35)/0.65]^2\} * \{1.0 - [(S_w - 0.35)/0.65]\}^2 \quad (41)$$

TABLE 2 - DATA FOR EXAMPLE WITH CONVERSION

porosity	ϕ	0.10
reservoir thermal conductivity	K_m	3.20×10^5 ergs/sec-cm°C
rock density	ρ_r	2.50 g/cm^3
rock specific heat	c_r	1.01×10^7 ergs/g°C
aquifer thickness	b	5.00×10^4 cm
initial pressure	p_i	4.38×10^7 dynes/cm ²
initial enthalpy	h_i	1.02×10^{10} ergs/g
initial temperature	T_i	236.12°C
initial density	ρ_i	0.82 g/cm^3
permeability	k	1.00×10^{-10} cm ²
discharge rate	Q	2.00×10^4 g/sec

Figure 7. Formated Data for Example 2.

```

EXAMPLE RUN WITH CONVERSION
10      1      10      12      18      1      7      1      1
500000.
1      1      1      1      1      1      1      1
20000.
50000.
.43808
1.024010
0.10-9
0.10-9
0.1
50000.
1      1      -20000.
3.205      0.00000      1.0107      2.5      0.000

```

These relationships may be found in the program at statement numbers PRP1230 - PRP1300. For problems with different functions, the user must change these statements. Note that experience has shown that these functions must be smooth and continuous or numerical oscillations may result.

At the end of 17 time steps (8.5×10^6 sec) the finite-difference model predicts that the water saturation in the first block is 0.96994; all other blocks are at a saturation of 1.0. For illustrative purposes results from the finite-element and finite-difference models (Faust and Mercer, 1976) for the five year simulation are compared in figures 8 and 9. In figure 8, pressure is plotted versus distance (origin is at the left end of the reservoir), for various simulation times. The specified times represent the duration of exploitation. In this example, the pressure drops rapidly in the early stages of production, and at the end of one month the first block has become two phase. When this occurs, the pressure continues to drop rapidly in the rest of the reservoir, but changes only slightly in the block containing the sink. This is expected, because once a block becomes two-phase, the pressure is maintained by the formation of steam. Also, note that once the system becomes two phase, the time step may be increased without causing any numerical problems. After 3 years of exploitation, the pressures in the entire reservoir have lowered to a point just slightly above the saturated-vapor pressure. Subsequent mass extraction results in reduced water saturations in elements near the sink, and pressures drop very slowly.

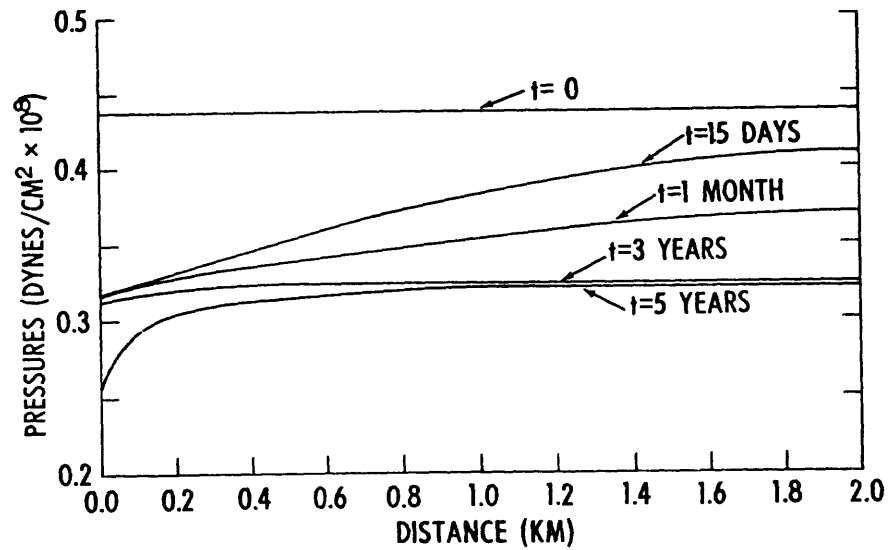


Figure 8.- Computed pressure distribution at various times for example 2. (After Faust and Mercer, 1976.)

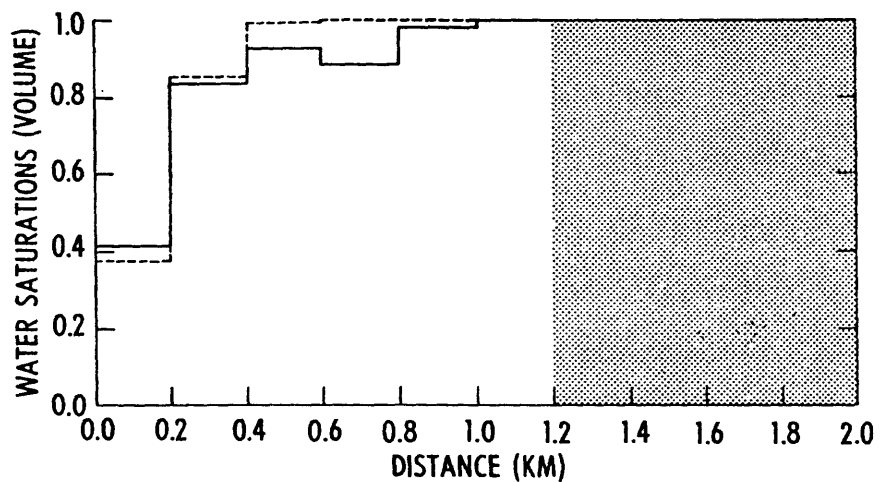


Figure 9. Computed water saturation distribution for example 2 after 5 years of exploitation. (Single-phase water indicated by shading; solid line: Galerkin finite-element solution; dashed line: finite-difference solution.) After Faust and Mercer, 1976.

Water saturation distributions at the end of 5 years of exploitation predicted by both the Galerkin- and finite-difference models are shown in figure 9. Note that the finite-element solution exhibits an oscillation in the saturation distribution. The upstream-weighting scheme used in the finite-difference model eliminates this oscillation.

NOTATION

Parameter	Coded Name	Description
b	DZ	reservoir thickness
c_r	PHFWT	rock specific heat
h	H	enthalpy
h_r	HROCK	rock enthalpy
h_s	HS	steam enthalpy
h_w	HW	water enthalpy
K_m	XKC	medium thermal conductivity
K_r	CØND	confining bed thermal conductivity
k	XK	x- permeability
	YK	y- permeability
k_r	XKW	water relative permeability
	XKS	steam relative permeability
p	P	pressure
q_m^*	Q	mass source term
q_h^*	QH	energy source term
q_{ll}	CQ	vertical conductive energy source term
S_w	SW1	water volume saturation
T	TEMP2	temperature
t	TIME	simulation time
β	BETA	rock compressibility
μ_s	VS	steam viscosity

Parameter	Coded Name	Description
μ_w	VW	water viscosity
ρ	DEN2	density
ρ_r	DF	rock density
ρ_s	DS	steam density
ρ_w	DW	water density
ϕ	PHI	porosity

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PROGRAM LISTING

C	MAIN PROGRAM	MNP	10
C	*****	MNP	20
	IMPLICIT REAL*8(A-H,O-Z)	MNP	30
C		MNP	40
C	PURPOSE: TO SIMULATE VAPOR- AND LIQUID-DOMINATED GEOTHERMAL	MNP	50
C	RESERVOIRS USING FINITE DIFFERENCE TECHNIQUES	MNP	60
C	PROGRAMED BY CHARLES H. FAUST AND JAMES W. MERCER	MNP	70
C	U. S. GEOLOGICAL SURVEY	MNP	80
C	1975-1976	MNP	90
C	-----	MNP	100
C		MNP	110
C	TO MINIMIZE CORE, DIMENSION A AND R FOR EACH PROBLEM:	MNP	120
C	A(NBB,MBE), R(NBB)	MNP	130
C	DIMENSION A(300,43), R(300)	MNP	140
C		MNP	150
	COMMON /INPUT/ PHI(20,10),XK(20,10),YK(20,10),P(20,10),H(20,10),X	MNP	160
	1400),X1(400),NP(20,10),NPP(200,2),DX(20),DY(10),DZ(20,10),Q(20,10)	MNP	170
	COMMON /CONTROL/ NK,NX,NXX,NY,NYY,NB,NBB,NT,DELT,TIME,PHFWT,DF,XKC,	MNP	180
	ICOND,COEF,BETA,IPRT	MNP	190
	COMMON /WORK/ AX(21,10),BX(21,10),EX(21,10),AY(20,11),BY(20,11),EY	MNP	200
	1(20,11),TX(21,10),TXK(21,10),TY(20,11),TYK(20,11),XM(20,10),XMASS	MNP	210
	220,10),EN(20,10),ENERGY(20,10),C(20,10),D(20,10),F(20,10),G(20,10)	MNP	220
	3,QF(20,10),XN(20,10),IM(20,10),DTP(20,10),DTH(20,10),PHIC(20,10),P	MNP	230
	4OLD(20,10)	MNP	240
	COMMON /EXTRA/ MBW,MBE	MNP	250
	COMMON /CHECK/ IND(200),INCOLD(200)	MNP	260
C	-----	MNP	270
C		MNP	280
C	GET DATA -	MNP	290
C	CALL GDATA(IOPT)	MNP	300
C	*****	MNP	310
	NKK=NK	MNP	320
C		MNP	330
C	FOR DIMENSIONING -	MNP	340
	NBBB=NBB	MNP	350
	MBED=MBE	MNP	360
C		MNP	370
C	CALCULATE TRANSMISSIBILITY TERMS -	MNP	380
	CALL TCALC(DY,DX,DZ,XK,YK,TY,TYK,TX,TAN,XKC,NY,NX,NYY,NXX)	MNP	390
C	*****	MNP	400
C		MNP	410
C	CALCULATE BANDWIDTH -	MNP	420
	CALL MATR(NP,NY,NX,MBE,MBW)	MNP	430
C	*****	MNP	440
C		MNP	450
C	CHECK INITIAL PHASE CONDITIONS	MNP	460
C	COMPUTE THERMODYNAMIC REGION -	MNP	470
	CALL PHREG(IND)	MNP	480
C	*****	MNP	490
	DO 10 K=1,NB	MNP	500
	10 INCOLD(K)=IND(K)	MNP	510
C		MNP	520

C	CALCULATE INITIAL BALANCE -	MNP 530
	CALL BALNCE(0,NKK,PCEE)	MNP 540
C	*****	MNP 550
C		MNP 560
C		MNP 570
C	TIME LOOP -	MNP 580
	DO 180 L=1,NT	MNP 590
C		MNP 600
C	ITERATION LOOP -	MNP 610
	DO 130 KKK=1,NK	MNP 620
C		MNP 630
C	CALCULATE PROPERTY COEFFICIENTS -	MNP 640
	CALL PRPTY(L,KKK)	MNP 650
C	*****	MNP 660
C		MNP 670
C	INITIALIZE BOUNDARY ARRAYS -	MNP 680
	DO 20 I=1,NX	MNP 690
	AY(I,1)=0.D0	MNP 700
	BY(I,1)=0.D0	MNP 710
	EY(I,1)=0.D0	MNP 720
	AY(I,NYY)=0.D0	MNP 730
	BY(I,NYY)=0.D0	MNP 740
	20 EY(I,NYY)=0.D0	MNP 750
C		MNP 760
	DO 30 J=1,NY	MNP 770
	AX(1,J)=0.D0	MNP 780
	BX(1,J)=0.D0	MNP 790
	EX(1,J)=0.D0	MNP 800
	AX(NXX,J)=0.D0	MNP 810
	BX(NXX,J)=0.D0	MNP 820
	30 EX(NXX,J)=0.D0	MNP 830
C		MNP 840
	DO 50 J=1,NY	MNP 850
	DO 50 I=2,NX	MNP 860
C	FOR UPSTREAM WEIGHTING -	MNP 870
	ALPHA=1.D0	MNP 880
	IF (P(I-1,J).GT.P(I,J)) ALPHA=0.D0	MNP 890
	IF (IOPT.EQ.1) GO TO 40	MNP 900
C	FOR MIDPOINT WEIGHTING -	MNP 910
	ALPHA=DX(I)/(DX(I)+DX(I-1))	MNP 920
	40 EX(I,J)=(ALPHA*XN(1,J)+(1.0-ALPHA)*XN(I-1,J))*TX(I,J)	MNP 930
	AX(I,J)=(ALPHA*DTP(I,J)+(1.0-ALPHA)*DTP(I-1,J))*TXK(I,J)+(ALPHA*TM	MNP 940
	1(I,J)+(1.0-ALPHA)*TM(I-1,J))*TX(I,J)	MNP 950
	50 BX(I,J)=(ALPHA*DTH(I,J)+(1.0-ALPHA)*DTH(I-1,J))*TXK(I,J)	MNP 960
C		MNP 970
	DO 70 I=1,NX	MNP 980
	DO 70 J=2,NY	MNP 990
	ALPHA=1.D0	MNP1000
	IF (P(I,J-1).GT.P(I,J)) ALPHA=0.D0	MNP1010
	IF (IOPT.EQ.1) GO TO 60	MNP1020
	ALPHA=DY(J)/(DY(J)+DY(J-1))	MNP1030
	60 EY(I,J)=(ALPHA*XN(I,J)+(1.0-ALPHA)*XN(I,J-1))*TY(I,J)	MNP1040

	AY(I,J)=(ALPHA*DTP(I,J)+(1.0-ALPHA)*DTP(I,J-1))*TYK(I,J)+(ALPHA*TM	MNP1050
	1(I,J)+(1.0-ALPHA)*TM(I,J-1))*TY(I,J)	MNP1060
	70 BY(I,J)=(ALPHA*DTH(I,J)+(1.0-ALPHA)*DTH(I,J-1))*TYK(I,J)	MNP1070
C		MNP1080
C	FORM FINAL MATRIX EQUATION -	MNP1090
	CALL FORMEQ(A,R,NBBD,MBED)	MNP1100
C	*****	MNP1110
	IMHALF=(MBW-1)/2	MNP1120
C		MNP1130
C	TRIANGULARIZE -	MNP1140
	CALL SOLVE(1,A,R,NBB,IMHALF,NBBD,MBED)	MNP1150
C	*****	MNP1160
C		MNP1170
C	SOLVE -	MNP1180
	CALL SOLVE(2,A,R,NBB,IMHALF,NBBD,MBED)	MNP1190
C	*****	MNP1200
	DO 80 K=1,NB	MNP1210
	X1(2*K-1)=X1(2*K-1)+R(2*K-1)	MNP1220
80	X1(2*K)=X1(2*K)+R(2*K)	MNP1230
	IF (KKK.NE.1) GO TO 110	MNP1240
85	CONTINUE	MNP1245
	CALL PHREG(IND)	MNP1250
C	*****	MNP1260
C		MNP1270
C	DID A CONVERSION OCCURE? -	MNP1280
	DO 100 K=1,NB	MNP1290
100	INDOLD(K)=IND(K)	MNP1450
	GO TO 105	MNP1455
110	CONTINUE	MNP1460
	IF (KKK.GE.4) GO TO 85	MNP1465
105	CONTINUE	MNP1467
	DO 120 K=1,NB	MNP1470
	I=NPP(K,1)	MNP1480
	J=NPP(K,2)	MNP1490
	P(I,J)=X1(2*K-1)	MNP1500
120	H(I,J)=X1(2*K)	MNP1510
	WRITE (6,190) KKK	MNP1520

C		NNP1530
C	CALCULATE MASS AND HEAT BALANCE -	NNP1540
	CALL BALNCE(1,KKK,PCEE)	NNP1550
C	*****	NNP1560
	ERR=DABS(PCEE)	NNP1570
C	CHECK ERROR OF ENERGY BALANCE TO DETERMINE NUMBER OF ITERATIONS -	NNP1580
	IF (ERR.LT.0.02) GO TO 140	NNP1590
130	CONTINUE	NNP1600
	GO TO 160	NNP1610
140	CONTINUE	NNP1620
	DO 150 I=1,NX	NNP1630
	DO 150 J=1,NY	NNP1640
	XMASS(I,J)=XM(I,J)	NNP1650
150	ENERGY(I,J)=EN(I,J)	NNP1660
160	CONTINUE	NNP1670
C		NNP1680
C	END ITERATION LOOP	NNP1690
	DO 170 K=1,NBB	NNP1700
170	X(K)=X1(K)	NNP1710
	TIME=TIME+DELT	NNP1720
C		NNP1730
C	PRINT RESULTS -	NNP1740
	CALL PDATA(P,H,TIME,L,NY,NX)	NNP1750
C	*****	NNP1760
180	CONTINUE	NNP1770
C		NNP1780
C	END TIME LOOP	NNP1790
	STOP	NNP1800
C		NNP1810
190	FORMAT (//15X,16HITERATION NUMBER,I5)	NNP1820
	END	NNP1830-

	SUBROUTINE GDATA(IOPT)	DAT 10
C	*****	DAT 20
	IMPLICIT REAL*8(A-H,O-Z)	DAT 30
C		DAT 40
C	CALLED FROM MAIN	DAT 50
C	PURPOSE: TO READ AND WRITE PROBLEM INFORMATION	DAT 60
C	-----	DAT 70
	DIMENSION TITLE(20)	DAT 80
C		DAT 90
	COMMON /INPUT/ PHI(20,10),XK(20,10),YK(20,10),P(20,10),H(20,10),X(DAT 100	
	1400),X1(400),NP(20,10),NPP(200,2),DX(20),DY(10),DZ(20,10),Q(20,10)DAT 110	
	COMMON /CONTRU/ NK,NX,NXX,NY,NYY,NB,NBB,NT,DELT,TIME,PHFWT,DF,XKC,DAT 120	
	1COND,COEF,BETA,IPRT	DAT 130
	COMMON /WORK/ AX(21,10),BX(21,10),EX(21,10),AY(20,11),BY(20,11),EYDAT 140	
	1(20,11),TX(21,10),TXK(21,10),TY(20,11),TYK(20,11),XM(20,10),XMASS(DAT 150	
	220,10),EN(20,10),ENERGY(20,10),C(20,10),D(20,10),F(20,10),G(20,10)DAT 160	
	3,QH(20,10),XN(20,10),IM(20,10),DTP(20,10),DTH(20,10),PHIC(20,10),PDAT 170	
	4OLD(20,10)	DAT 180
	COMMON /EXTRA/ MBW,MBE	DAT 190
C	-----	DAT 200
C		DAT 210
C	READ AND WRITE UNITS -	DAT 220
	NR=5	DAT 230
	NW=6	DAT 240
C		DAT 250
C	INITIALIZE SIMULATION TIME -	DAT 260
	TIME=0.00	DAT 270
C		DAT 280
C	READ AND WRITE TITLE OF PROBLEM -	DAT 290
	READ (NR,280) TITLE	DAT 300
	WRITE (NW,290)	DAT 310
	WRITE (NW,300) TITLE	DAT 320
C		DAT 330
C	READ AND WRITE FINITE DIFFERENCE INFORMATION -	DAT 340
	READ (NR,310) NX,NY,NB,NK,NT,NS,MBE,IOPT,IPRT	DAT 350
C	NX - NUMBER OF COLUMNS (X-DIRECTION)	DAT 360
C	NY - NUMBER OF ROWS (Y-DIRECTION)	DAT 370
C	NB - NUMBER OF NON-ZERO BLOCKS	DAT 380
C	NK - MAXIMUM NUMBER OF NEWTON ITERATIONS	DAT 390
C	NT - MAXIMUM NUMBER OF TIME STEPS	DAT 400
C	NS - NUMBER OF SOURCES	DAT 410
C	MBE - ESTIMATED BANDWIDTH	DAT 420
C	IOPT - READ 1 FOR UPSIDEAM WEIGHTING ON PRESSURE;	DAT 430
C	2 FOR MIDPOINT WEIGHTING	DAT 440
C	IPRT - NUMBER OF TIME STEPS BETWEEN PRINTING THERMO DATA	DAT 450
	WRITE (NW,320)	DAT 460
	WRITE (NW,330) NX,NY,NB,NK,NT,NS,MBE,IOPT,IPRT	DAT 470
C		DAT 480
	NXX=NX+1	DAT 490
	NYY=NY+1	DAT 500
	NBB=2*NB	DAT 510
C	NBE - TOTAL NUMBER OF EQUATIONS	DAT 520

C		DAT 530
C	TIME PARAMETERS -	DAT 540
	READ (NR,340) DELT	DAT 550
C	DELT - TIME STEP IN SECONDS	DAT 560
	WRITE (NW,370) DELT	DAT 570
C		DAT 580
C	DATA CODES -	DAT 590
	READ (NR,310) KOD1,KOD2,KOD3,KOD4,KOD5,KOD6,KOD7,KOD8,KOD9	DAT 600
C	KOD1 - READ 1 IF X-SPACING IS CONSTANT	DAT 610
C	KOD2 - READ 1 IF Y-SPACING IS CONSTANT	DAT 620
C	KOD3 - READ 1 IF INITIAL PRESSURE IS CONSTANT	DAT 630
C	KOD4 - READ 1 IF INITIAL ENTHALPY IS CONSTANT	DAT 640
C	KOD5 - READ 1 IF X-PERMEABILITY IS CONSTANT	DAT 650
C	KOD6 - READ 1 IF Y-PERMEABILITY IS CONSTANT	DAT 660
C	KOD7 - READ 1 IF INITIAL POROSITY IS CONSTANT	DAT 670
C	KOD8 - READ 1 IF RESERVOIR THICKNESS IS CONSTANT	DAT 680
C	KOD9 - READ 1 IF TEMPERATURE IS READ IN PLACE OF ENTHALPY	DAT 690
	WRITE (NW,260) KOD1,KOD2,KOD3,KOD4,KOD5,KOD6,KOD7,KOD8,KOD9	DAT 700
C		DAT 710
C	SPACING -	DAT 720
	IF (KOD1.EQ.1) GO TO 10	DAT 730
	READ (NR,340) (DX(I),I=1,NX)	DAT 740
	GO TO 30	DAT 750
	10 READ (NR,340) DX1	DAT 760
	DO 20 I=1,NX	DAT 770
	20 DX(I)=DX1	DAT 780
	30 WRITE (NW,350)	DAT 790
	WRITE (NW,390) (DX(I),I=1,NX)	DAT 800
C		DAT 810
	IF (KOD2.EQ.1) GO TO 40	DAT 820
	READ (NR,340) (DY(J),J=1,NY)	DAT 830
	GO TO 60	DAT 840
	40 READ (NR,340) DY1	DAT 850
	DO 50 J=1,NY	DAT 860
	50 DY(J)=DY1	DAT 870
	60 WRITE (NW,360)	DAT 880
	WRITE (NW,390) (DY(J),J=1,NY)	DAT 890
C		DAT 900
C	PRESSURE -	DAT 910
	WRITE (NW,380)	DAT 920
	CALL READ(P,KOD3,NY,NX)	DAT 930
C	*****	DAT 940
C		DAT 950
C	ENTHALPY -	DAT 960
	IF (KOD9.EQ.1) WRITE (NW,270)	DAT 970
	IF (KOD9.NE.1) WRITE (NW,400)	DAT 980
	CALL READ(H,KOD4,NY,NX)	DAT 990
C	*****	DAT1000
	IF (KOD9.NE.1) GO TO 100	DAT1010
C		DAT1020
C	TEMPERATURES READ (COMPRESSED WATER REGION ASSUMED)	DAT1030
C	COMPUTE ENTHALPY BY NEWTON-RAPHSON METHOD	DAT1040

DO 80 J=1,NY	DAT1050
DO 80 I=1,NX	DAT1060
IF (H(I,J).EQ.0.) GO TO 80	DAT1070
T=F(I,J)	DAT1080
H(I,J)=T*41841004.18	DAT1090
PP=P(I,J)*0.1**7	DAT1100
HH=H(I,J)*0.1**7	DAT1110
DO 70 JJ=1,4	DAT1120
T1=-2.41231+2.56222D-01*HH-9.31415D-03*PP*PP-2.2568D-05*HH*HH	DAT1130
DT=2.56222D-01-4.5136D-05*HH	DAT1140
DH=-(T1-T)/DT	DAT1150
HH=HH+DH	DAT1160
70 CONTINUE	DAT1170
H(I,J)=HH*10.**7	DAT1180
80 CONTINUE	DAT1190
WRITE (NW,400)	DAT1200
DO 90 J=1,NY	DAT1210
90 WRITE (NW,390) (H(I,J),I=1,NX)	DAT1220
100 CONTINUE	DAT1230
C	DAT1240
C X- AND Y-PERMEABILITY -	DAT1250
WRITE (NW,410)	DAT1260
CALL READ(XK,KOD5,NY,NX)	DAT1270
C *****	DAT1280
C	DAT1290
WRITE (NW,420)	DAT1300
CALL READ(YK,KOD6,NY,NX)	DAT1310
C *****	DAT1320
C	DAT1330
C POROSITY -	DAT1340
WRITE (NW,430)	DAT1350
CALL READ(PHI,KOD7,NY,NX)	DAT1360
C *****	DAT1370
C SAVE PRESSURE AND INITIAL POROSITY -	DAT1380
DO 110 I=1,NX	DAT1390
DO 110 J=1,NY	DAT1400
POD(I,J)=P(I,J)	DAT1410
110 PHIO(I,J)=PHI(I,J)	DAT1420
C	DAT1430
C RESERVOIR THICKNESS (BY BLOCKS) -	DAT1440
WRITE (NW,440)	DAT1450
CALL READ(DZ,KOD8,NY,NX)	DAT1460
C *****	DAT1470
C	DAT1480
C SOURCE/SINK (G/SEC) -	DAT1490
WRITE (NW,450)	DAT1500
DO 120 J=1,NY	DAT1510
DO 120 I=1,NX	DAT1520
120 Q(I,J)=0.D0	DAT1530
IF (NS.EQ.0) GO TO 140	DAT1540
DO 130 K=1,NS	DAT1550
READ (NR,460) I,J,Q(I,J)	DAT1560

130	WRITE (NW,470) I,J,Q(I,J)	DAT1570
C		DAT1580
C	ROCK PROPERTIES -	DAT1590
140	READ (NR,340) XKC,COND,PHFWT,DF,BETA	DAT1600
C	XKC - MEDIUM THERMAL CONDUCTIVITY	DAT1610
C	COND - CONFINING BED THERMAL CONDUCTIVITY	DAT1620
C	PHFWT - ROCK ENTHALPY DERIVATIVE W.R.T. TEMPERATURE	DAT1630
C	DF - ROCK DENSITY	DAT1640
C	BETA - ROCK COMPRESSIBILITY	DAT1650
	WRITE (NW,480) XKC,COND,PHFWT,DF,BETA	DAT1660
C		DAT1670
C	COMPUTE COEFFICIENT FOR CONDUCTIVE LEAKAGE -	DAT1680
	IF (COND.LT.0.1) GO TO 150	DAT1690
	COEF=DF*PHFWT/COND	DAT1700
	GO TO 160	DAT1710
150	COEF=0.00	DAT1720
160	CONTINUE	DAT1730
C		DAT1740
C	NUMBER GRID BLOCKS -	DAT1750
C	NP(I,J) - SEQUENCE NUMBERING OF BLOCKS I,J	DAT1760
	IBN=0	DAT1770
	DO 190 I=1,NX	DAT1780
	DO 180 J=1,NY	DAT1790
	IF (DZ(I,J).LT.0.001) GO TO 170	DAT1800
	IBN=IBN+1	DAT1810
	NP(I,J)=IBN	DAT1820
	GO TO 180	DAT1830
170	NP(I,J)=0	DAT1840
180	CONTINUE	DAT1850
190	CONTINUE	DAT1860
	WRITE (NW,240)	DAT1870
	DO 200 J=1,NY	DAT1880
200	WRITE (NW,250) (NP(I,J),I=1,NX)	DAT1890
C		DAT1900
C	COMPUTE I,J FOR EACH SEQUENTIAL BLOCK NUMBER -	DAT1910
	DO 220 I=1,NX	DAT1920
	DO 220 J=1,NY	DAT1930
	IJ=NP(I,J)	DAT1940
	IF (IJ.EQ.0) GO TO 220	DAT1950
	NPP(IJ,1)=I	DAT1960
	NPP(IJ,2)=J	DAT1970
	GO TO 220	DAT1980
220	CONTINUE	DAT2000
C		DAT2010
C	INITIALIZE SOLUTION VECTOR -	DAT2020
	DO 230 K=1,NB	DAT2030
	II=NPP(K,1)	DAT2040
	JJ=NPP(K,2)	DAT2050
	X(2*K-1)=P(II,JJ)	DAT2060
	X1(2*K-1)=P(II,JJ)	DAT2070
	X(2*K)=H(II,JJ)	DAT2080
	X1(2*K)=H(II,JJ)	DAT2090

230 CONTINUE	0AT2100
RETURN	0AT2110
C	0AT2120
240 FORMAT (11X,12HGRID NUMBERS/11X,12(1H-))	0AT2130
250 FORMAT (11X,16I5)	0AT2140
260 FORMAT (//////11X,5HCODES/11X,5(1H-)/11X,9I5)	0AT2150
270 FORMAT (//////,11X,19HINITIAL TEMPERATURE/11X,19(1H-)/)	0AT2160
280 FORMAT (20A4)	0AT2170
290 FORMAT (1H1,///35X,25HSTEAM-WATER FLOW ANALYSIS//)	0AT2180
300 FORMAT (11X,70(1H*)//11X,20A4//11X,70(1H*)///)	0AT2190
310 FORMAT (16I5)	0AT2200
320 FORMAT (/11X,22HFINITE DIFFERENCE DATA/11X,22(1H-)/)	0AT2210
330 FORMAT (1H,10X,11HNUMBER OF -,2X,7HCOLUMNS,123/21X,1H-,2X,4HROWS,0AT2220	
1126/21X,1H-,2X,15HNON-ZERO BLOCKS,115/21X,1H-,2X,18HMAXIMUM ITERATION	0AT2230
2IONS,112/21X,1H-,2X,18HMAXIMUM TIME STEPS,112/21X,1H-,2X,7HSOURCES	0AT2240
3,123/21X,1H-,2X,19HESTIMATED BANDWIDTH,111/21X,1H-,2X,16HWEIGHTING	0AT2250
4 OPTION,114/21X,1H-,2X,15HPRINTING OPTION,115///)	0AT2260
340 FORMAT (8G10.0)	0AT2270
350 FORMAT (//////,11X,22HSPACING IN X-DIRECTION/11X,22(1H-)/)	0AT2280
360 FORMAT (//////,11X,22HSPACING IN Y-DIRECTION/11X,22(1H-)/)	0AT2290
370 FORMAT (////,11X,15HTIME PARAMETERS/11X,15(1H-)/11X,28HINITIAL TIME	0AT2300
1E STEP IN SECONDS,G22.8/)	0AT2310
380 FORMAT (//////,11X,16HINITIAL PRESSURE/11X,16(1H-)/)	0AT2320
390 FORMAT (/11X,8(G12.5,2X)))	0AT2330
400 FORMAT (//////,11X,16HINITIAL ENTHALPY/11X,16(1H-)/)	0AT2340
410 FORMAT (//////,11X,14HX-PERMEABILITY/11X,14(1H-)/)	0AT2350
420 FORMAT (//////,11X,14HY-PERMEABILITY/11X,14(1H-)/)	0AT2360
430 FORMAT (//////,11X,16HINITIAL POROSITY/11X,16(1H-)/)	0AT2370
440 FORMAT (//////,11X,19HRESERVOIR THICKNESS/11X,19(1H-)/)	0AT2380
450 FORMAT (//////,11X,7HSOURCES/11X,7(1H-)/)	0AT2390
460 FORMAT (2J5,G15.0)	0AT2400
470 FORMAT (11X,2I5,G15.8)	0AT2410
480 FORMAT (/11X,15HROCK PROPERTIES/11X,15(1H-)/11X,28HMEDIUM THERMAL	0AT2420
1CONDUCTIVITY-G17.5/11X,35HCONFINING BED THERMAL CONDUCTIVITY-G10.30	0AT2430
2/11X,25HROCK ENTHALPY DERIVATIVE-G20.5/11X,13HROCK DENSITY-G32.5/10	0AT2440
31X,ROCK COMPRESSIBILITY-,G24.5/)	0AT2450
END	0AT2460-

	SUBROUTINE READ(DUM,KODE,NY,NX)	REC 10
C	*****	REC 20
	IMPLICIT REAL*8(A-H,O-Z)	REC 30
C		REC 40
C	CALLED FROM GDATA	REC 50
C	PURPOSE: TO READ TWO-DIMENSIONAL ARRAYS	REC 60
C	-----	REC 70
	DIMENSION DUM(20,10)	REC 80
C	-----	REC 90
	NR=5	REC 100
	NW=6	REC 110
	IF (KODE.EQ.1) GO TO 20	REC 120
	DO 10 J=1,NY	REC 130
10	READ (NR,70) (DUM(I,J),I=1,NX)	REC 140
	GO TO 40	REC 150
20	READ (NR,70) DUM1	REC 160
	DO 30 J=1,NY	REC 170
	DO 30 I=1,NX	REC 180
30	DUM(I,J)=DUM1	REC 190
40	DO 50 J=1,NY	REC 200
50	WRITE (NW,60) (DUM(I,J),I=1,NX)	REC 210
	RETURN	REC 220
C		REC 230
	60 FORMAT (/(11X,8(G12.5,2X)))	REC 240
	70 FORMAT (8G10.0)	REC 250
	END	REC 260-

	SUBROUTINE TCALC(DY,DX,DZ,XK,YK,TY,TK,TX,TK,XKC,NY,NX,NYY,NXX)	TCA 10
C	*****	TCA 20
	IMPLICIT REAL*8(A-H,O-Z)	TCA 30
C		TCA 40
C	CALLED FROM MAIN	TCA 50
C	PURPOSE: TO COMPUTE TRANSMISSIBILITY TERMS -	TCA 60
C	-----	TCA 70
	DIMENSION DY(10), DX(20), DZ(20,10), XK(20,10), YK(20,10), TY(20,1	TCA 80
	11), TK(20,11), TX(21,10), TK(21,10)	TCA 90
C	-----	TCA 100
C		TCA 110
C	COMPUTE TRANSMISSIBILITY TERMS IN THE X-DIRECTION -	TCA 120
	DO 10 J=1,NY	TCA 130
C	IF ONLY ONE COLUMN, SKIP CALCULATIONS -	TCA 140
	IF (NX.EQ.1) GO TO 20	TCA 150
	DO 10 I=2,NX	TCA 160
	TXC=DY(J)*DZ(I-1,J)/DX(I-1)	TCA 170
	TXD=DY(J)*DZ(I,J)/DX(I)	TCA 180
	TXA=TXC*XK(I-1,J)	TCA 190
	TXB=TXD*XK(I,J)	TCA 200
	TTI=TXA+TXB	TCA 210
	IF (TTI.EQ.0.0) GO TO 10	TCA 220
C	PERMEABILITY TERM -	TCA 230
	TX(I,J)=2.0*TXA*TXB/TTI	TCA 240
C	HEAT CONDUCTION TERM -	TCA 250
	TK(I,J)=2.0*TXC*TXD/(TXC+TXD)*XKC	TCA 260
10	CONTINUE	TCA 270
20	CONTINUE	TCA 280
C		TCA 290
C	COMPUTE TRANSMISSIBILITY TERMS IN THE Y-DIRECTION -	TCA 300
	DO 30 I=1,NX	TCA 310
	IF (NY.EQ.1) GO TO 40	TCA 320
	DO 30 J=2,NY	TCA 330
	TYC=DX(I)*DZ(I,J-1)/DY(J-1)	TCA 340
	TYD=DX(I)*DZ(I,J)/DY(J)	TCA 350
	TYA=TYC*YK(I,J-1)	TCA 360
	TYB=TYD*YK(I,J)	TCA 370
	TTT=TYA+TYB	TCA 380
	IF (TTT.EQ.0.0) GO TO 30	TCA 390
	TY(I,J)=2.0*TYA*TYB/TTT	TCA 400
	TK(I,J)=2.0*TYC*TYD/(TYC+TYD)*XKC	TCA 410
30	CONTINUE	TCA 420
40	CONTINUE	TCA 430
C		TCA 440
C	SET TRANSMISSIBILITY OF BOUNDARY BLOCKS (REGULAR RECTANGULAR MESH)	TCA 450
C	TO ZERO (NO-FLOW) -	TCA 460
	DO 50 I=1,NX	TCA 470
	TY(I,1)=0.00	TCA 480
	TK(I,1)=0.00	TCA 490
	TY(I,NYY)=0.00	TCA 500
50	TK(I,NYY)=0.00	TCA 510
C		TCA 520

DO 60 J=1,NY	TCA 530
TX(1,J)=0.D0	TCA 540
TXK(1,J)=0.D0	TCA 550
TX(NXX,J)=0.D0	TCA 560
60 TXK(NXX,J)=0.D0	TCA 570
C	TCA 580
C SET TRANSMISSIBILITY OF BOUNDARY BLOCKS (EXTERNAL AND INTERNAL,	TCA 590
C IRREGULAR MESH) TO ZERO -	TCA 600
DO 80 I=1,NX	TCA 610
DO 70 J=1,NY	TCA 620
IF (DZ(I,J).GT.0.D0) GO TO 70	TCA 630
TX(I+1,J)=0.D0	TCA 640
TXK(I+1,J)=0.D0	TCA 650
TY(I,J+1)=0.D0	TCA 660
TYK(I,J+1)=0.D0	TCA 670
TXK(I,J)=0.D0	TCA 680
TX(I,J)=0.D0	TCA 690
TYK(I,J)=0.D0	TCA 700
TY(I,J)=0.D0	TCA 710
70 CONTINUE	TCA 720
80 CONTINUE	TCA 730
RETURN	TCA 740
END	TCA 750-

	SUBROUTINE MATH(NP,NY,NX,MBE,MBW)	MAT 10
C	*****	MAT 20
	IMPLICIT REAL*8(A-H,O-Z)	MAT 30
C		MAT 40
C	CALLED FROM MAIN	MAT 50
C	PURPOSE: COMPUTE MATRIX BANDWIDTH	MAT 60
C	-----	MAT 70
	DIMENSION N(5), NP(20,10)	MAT 80
C	-----	MAT 90
C		MAT 100
C	COMPUTE MAXIMUM DIFFERENCE BETWEEN SEQUENTIAL BLOCK NUMBERS	MAT 110
C	OF ADJACENT BLOCKS -	MAT 120
	MM=0	MAT 130
	DO 80 I=1,NX	MAT 140
	DO 70 J=1,NY	MAT 150
	DO 10 KK=1,4	MAT 160
10	N(KK)=0	MAT 170
	I1=I-1	MAT 180
	I2=I+1	MAT 190
	J1=J-1	MAT 200
	J2=J+1	MAT 210
	IF (I1.EQ.0) GO TO 20	MAT 220
	N(1)=NP(I1,J)	MAT 230
20	CONTINUE	MAT 240
	IF (I2.GT.NX) GO TO 30	MAT 250
	N(3)=NP(I2,J)	MAT 260
30	CONTINUE	MAT 270
	IF (J1.EQ.0) GO TO 40	MAT 280
	N(2)=NP(I,J1)	MAT 290
40	CONTINUE	MAT 300
	IF (J2.GT.NY) GO TO 50	MAT 310
	N(4)=NP(I,J2)	MAT 320
50	N(5)=NP(I,J)	MAT 330
	IF (N(5).EQ.0) GO TO 70	MAT 340
	DO 60 K=1,4	MAT 350
	IF (N(K).EQ.0) GO TO 60	MAT 360
C	COMPUTE DIFFERENCE -	MAT 370
	NN=N(5)-N(K)	MAT 380
	IF (NN.LT.0) NN=-NN	MAT 390
C	COMPUTE MAXIMUM DIFFERENCE -	MAT 400
	IF (NN.GT.MM) MM=NN	MAT 410
60	CONTINUE	MAT 420
70	CONTINUE	MAT 430
80	CONTINUE	MAT 440
C	COMPUTE BANDWIDTH -	MAT 450
	MBW=2*(2*MM+1)+1	MAT 460
	PRINT 90, MBW,MBE	MAT 470
	RETURN	MAT 480
C		MAT 490
90	FORMAT (//11X,'MAXIMUM BANDWIDTH IS ',I4,2X,'COMPARED TO ESTIMATED	MAT 500
	1 BANDWIDTH OF ',I4///)	MAT 510
	END	MAT 520-

	SUBROUTINE PRPTY(L,KKK)	PRP	10
C	*****	PRP	20
	IMPLICIT REAL*8(A-H,O-Z)	PRP	30
C		PRP	40
C	CALLED FROM MAIN	PRP	50
C	PURPOSE: TO COMPUTE THERMODYNAMIC PROPERTIES	PRP	60
C	-----	PRP	70
	DIMENSION SW1(20,10), TEMP2(20,10), DEN2(20,10)	PRP	80
	DIMENSION CQ(20,10)	PRP	90
C		PRP	100
	COMMON /INPUT/ PHI(20,10), XK(20,10), YK(20,10), P(20,10), H(20,10), X(PRP	PRP	110
	1400), X1(400), NP(20,10), NPP(200,2), DX(20), DY(10), DZ(20,10), G(20,10) PRP	PRP	120
	COMMON /CONTRO/ NK, NX, NXX, NY, NYY, NB, NBB, NT, DELT, TIME, PHFWT, UF, XKC, PRP	PRP	130
	1COND, COEF, BETA, IPRT	PRP	140
	COMMON /WORK/ AX(21,10), BX(21,10), EX(21,10), AY(20,11), BY(20,11), EY PRP	PRP	150
	1(20,11), TX(21,10), TXK(21,10), TY(20,11), TYK(20,11), XM(20,10), XMASS PRP	PRP	160
	220,10), EN(20,10), ENERGY(20,10), C(20,10), D(20,10), F(20,10), G(20,10) PRP	PRP	170
	3, QH(20,10), XN(20,10), TM(20,10), DTP(20,10), DTH(20,10), PHIC(20,10), PPRP	PRP	180
	4OLD(20,10)	PRP	190
	COMMON /CHECK/ IND(200), INDOLD(200)	PRP	200
C	-----	PRP	210
C		PRP	220
C	STATEMENT FUNCTIONS FOR THERMODYNAMIC PROPERTIES	PRP	230
C		PRP	240
	F1(PX,HX)=1.00207+4.42007D-4*PX-5.47450D-5*HX+5.02875D-7*HX*PX-1.2 PRP	PRP	250
	14791D-7*HX*HX	PRP	260
	F2(PX,HX)=-2.41231+2.56222D-1*HX-9.31415D-3*PX*PX-2.2568D-5*HX*HX PRP	PRP	270
	F3(PX,HX)=-2.26162D-5+0.0438441D0*PX-1.79088D-5*PX*HX+3.69276D-3*PRP	PRP	280
	1X*PX*PX*PX+5.17644D-13*HX*HX*HX*PX	PRP	290
	F4(PX,HX)=-374.669D0+47.9921D0*PX-0.6336D0*PX*PX+7.39386D-5*PX*HX PRP	PRP	300
	1X-3.3372D6/HX/HX/PX/PX+0.0357154D0/PX/PX/PX-1.1725D-9*HX*HX*HX*PX-PRP	PRP	310
	22.26861D15/HX/HX/HX/HX	PRP	320
C		PRP	330
C	F1 - DENSITY, COMPRESSED WATER REGION	PRP	340
C	F2 - TEMPERATURE, COMPRESSED WATER REGION	PRP	350
C	F3 - DENSITY, SUPER HEATED STEAM REGION	PRP	360
C	F4 - TEMPERATURE, SUPER HEATED STEAM REGION	PRP	370
	NKK=NK	PRP	380
	IF (L.NE.1) GO TO 20	PRP	390
	IF (KKK.NE.1) GO TO 20	PRP	400
C		PRP	410
C	INITIALIZE ARRAYS -	PRP	420
	DO 10 I=1,NX	PRP	430
	DO 10 J=1,NY	PRP	440
	XN(I,J)=0.D0	PRP	450
	TM(I,J)=0.D0	PRP	460
	C(I,J)=0.D0	PRP	470
	D(I,J)=0.D0	PRP	480
	F(I,J)=0.D0	PRP	490
	G(I,J)=0.D0	PRP	500
	QH(I,J)=0.D0	PRP	510
	DTP(I,J)=0.D0	PRP	520

	DTH(I,J)=0.00	PRP 530
	SW1(I,J)=0.00	PRP 540
	DEN2(I,J)=0.00	PRP 550
	TEMP2(I,J)=0.00	PRP 560
10	CONTINUE	PRP 570
20	CONTINUE	PRP 580
	DO 80 I=1,NX	PRP 590
	DO 80 J=1,NY	PRP 600
	IF (DZ(I,J).EQ.0.00) GO TO 80	PRP 610
	PP=P(I,J)	PRP 620
	HH=H(I,J)	PRP 630
	PP=PP*0.1**7	PRP 640
	HH=HH*0.1**7	PRP 650
C		PRP 660
	K=AP(I,J)	PRP 670
	IF (IND(K)) 30,40,50	PRP 700
30	CONTINUE	PRP 710
C		PRP 720
C		PRP 730
C	COMPRESSED WATER REGION -	PRP 740
C		PRP 750
	DW=F1(PP,HH)	PRP 760
	TEMP=F2(PP,HH)	PRP 770
	PDWP=4.42607D-11+5.02875D-14*HH	PRP 780
	PDWH=-5.47456D-12+5.02875D-14*PP-2.49582D-14*HH	PRP 790
	PTWP=-1.86283D-9*PP	PRP 800
	PTWH=2.56222D-8-4.5136D-12*HH	PRP 810
C	WATER VISCOSITY -	PRP 820
C	1967 ASME STEAM TABLES FORMULA (P. 74) -	PRP 830
	VW=1.0D-6*(241.4*10.** (247.8/(TEMP+133.15)))	PRP 840
C		PRP 850
C	COMPUTE EQUATION COEFFICIENTS -	PRP 860
C	SPACE -	PRP 870
	AN(I,J)=DW/VW	PRP 880
	TM(I,J)=DW*HH/VW*10.**7	PRP 890
	UTH(I,J)=PTWH	PRP 900
	UTF(I,J)=PTWP	PRP 910
C	TIME -	PRP 920
	C(I,J)=PDWP*PHI(I,J)*HH*10.**7+PHFWT*PIWP*DF*(1.0-PHI(I,J))	PRP 930
	C(I,J)=C(I,J)+DW*HH*1.07*BETA*PHIO(I,J)-PHIO(I,J)*BETA*DT*PHFWT*TEMP	PRP 940
IMP		PRP 950
	D(I,J)=PDWH*PHI(I,J)*HH*10.**7+PHFWT*PIWH*DF*(1.0-PHI(I,J))+DW*PHI	PRP 960
1(I,J)		PRP 970
	F(I,J)=PHI(I,J)*PDWP+U**BETA*PHIO(I,J)	PRP 980
	G(I,J)=PHI(I,J)*PDWH	PRP 990
C		PRP1000
	SW1(I,J)=1.00	PRP1010
	TEMP2(I,J)=TEMP	PRP1020
	DEN2(I,J)=DW	PRP1030
C	HEAT DISCHARGE -	PRP1040
	QH(I,J)=Q(I,J)*HH*10.**7	PRP1050
	GO TO 60	PRP1060

	40 CONTINUE	PRP1070
C		PRP1080
C		PRP1090
C	TWO-PHASE REGION -	PRP1100
	HW=730.984+129.239*PP-10.0333*PP*PP+0.39881*PP*PP*PP	
1	-99.0697/PP+12.9267/PP/PP-0.628359/PP/PP/PP	
	HS=2822.82-39.952/PP+2.54342/PP/PP-0.938879*PP*PP	PRP1110
	TEMP=F2(PP,HW)	PRP1120
	DW=F1(PP,HW)	PRP1130
	DS=F3(PP,HS)	PRP1140
C	WATER SATURATION -	PRP1150
	SW=DS*(HS-HH)/(HH*(DW-US)-(HW*DW-HS*DS))	PRP1160
	SST=1.0-SW	PRP1170
	SW0=SW	PRP1180
C	VISCOSITIES -	PRP1190
C	1967 ASME STEAM TABLES FORMULA (P. 74) -	PRP1200
	VW=1.0E-06*(241.4*10.**((247.8/(TEMP+133.15)))	PRP1210
	VS=1.0E-06*(.407*TEMP+80.4)	PRP1220
C	RELATIVE PERMEABILITY (WATER) -	PRP1230
	XKW=((SW-0.35)/0.65)**4	PRP1240
C	RELATIVE PERMEABILITY (STEAM) -	PRP1250
	XKS=(1.0-((SW-0.35)/0.65)**2)*(1.0-((SW-0.35)/0.65))**2	PRP1260
	IF (SW.LT.0.3) XKW=0.0	PRP1270
	IF (SW.LT.0.3) XKS=1.0	PRP1280
	IF (SW.GT.0.95) XKW=1.0	PRP1290
	IF (SW.GT.0.95) XKS=0.0	PRP1300
	DEN=DW*SW+SST*DS	PRP1310
	HHH=HH*1.001D0	PRP1320
	SW=DS*(HS-HHH)/(HHH*(DW-US)-(HW*DW-HS*US))	PRP1330
	SST=1.0-SW	PRP1340
	DEN1=DW*SW+DS*SST	PRP1350
	PDWH=(DEN1-DEN)/(HHH-HH)*1.0-7	PRP1360
	PPP=PP*.999D0	PRP1370
	HHW=730.984+129.239*PPP-10.0333*PPP*PPP+0.39881*PPP*PPP*PPP	
1	-99.0697/PPP+12.9267/PPP/PPP-0.628359/PPP/PPP/PPP	
	HHS=2822.82-39.952/PPP+2.54342/PPP/PPP-0.938879*PPP*PPP	PRP1400
	T1=F2(PPP,HHW)	PRP1410
	DDW=F1(PPP,HHW)	PRP1420
	DDS=F3(PPP,HHS)	PRP1430
	SW=DDS*(HHS-HH)/(HH*(DDW-DDS)-(HHW*DDW-HHS*DDS))	PRP1440
	SST=1.0-SW	PRP1450
	DEN1=DDW*SW+DDS*SST	PRP1460
	PDWP=(DEN1-DEN)/(PPP-PP)*1.0-7	PRP1470
	TEMP1=T1	PRP1480
	PTWP=(TEMP1-TEMP)/(PPP-PP)*1.0-7	PRP1490
	SW=SW0	PRP1500
C		PRP1510
C	SPACE -	PRP1520
	XN(I,J)=XKW*DW/VW+XKS*US/VS	PRP1530
	TM(I,J)=(XKW*DW*HW/VW+XKS*DS*HS/VS)*10.**7	PRP1540
	DTP(I,J)=PTWP	PRP1550
	DTM(I,J)=0.0	PRP1560

C	TIME -	PRP1570
	C(I,J)=PDWP*PHI(I,J)*HH*10.**7+PHFWT*PTWP*DF*(1.0-PHI(I,J))	PRP1580
	C(I,J)=C(I,J)+DEN*HH*1.07*BETA*PHIO(I,J)-PHIO(I,J)*BETA*DF*PHFWT*TEMP	PRP1590
	TEMP	PRP1600
	D(I,J)=PDWH*PHI(I,J)*HH*10.**7+DEN*PHI(I,J)	PRP1610
	F(I,J)=PHI(I,J)*PDWP+DEN*8BETA*PHIO(I,J)	PRP1620
	G(I,J)=PHI(I,J)*PDWH	PRP1630
C		PRP1640
	SW1(I,J)=SW	PRP1650
	TEMP2(I,J)=TEMP	PRP1660
	DEN2(I,J)=DEN	PRP1670
	QH(I,J)=Q(I,J)*(HW+(HS-HW)*XKS/(XKS+VS*XKW/VW*DW/DS))*10.**7	PRP1680
	GO TO 60	PRP1690
	50 CONTINUE	PRP1700
C		PRP1710
C		PRP1720
C	SUPER-HEATED STEAM REGION -	PRP1730
	DS=F3(PP,HH)	PRP1740
	PDWH=-1.79088D-12*PP+1.552932D-19*HH*HH*PP	PRP1800
	PDWP=4.38441D-9-1.79088D-12*HH+1.477104D-14*PP*PP*PP+5.17644D-20*H	PRP1810
	1H*HH*HH	PRP1820
	HW=730.984+129.239*PP-10.0333*PP*PP+0.39881*PP*PP*PP	
1	-99.0697/PP+12.9267/PP/PP-0.628359/PP/PP/PP	
	HS=2822.82-39.952/PP+2.54342/PP/PP-0.938879*PP*PP	
	TT1=F4(PP,HH)	
	TT2=F4(PP,HS)	
	TT3=F2(PP,HW)	
	TEMP=TT1-TT2+TT3	
	HHH=HH*1.001D0	
	TT1=F4(PP,HHH)	
	TEMPH=TT1-TT2+TT3	
	PPP=PP*0.999D0	
	HW=730.984+129.239*PPP-10.0333*PPP*PPP+0.39881*PPP*PPP*PPP	
1	-99.0697/PPP+12.9267/PPP/PPP-0.628359/PPP/PPP/PPP	
	HS=2822.82-39.952/PPP+2.54342/PPP/PPP-0.938879*PPP*PPP	
	TT1=F4(PPP,HH)	
	TT2=F4(PPP,HS)	
	TT3=F2(PPP,HW)	
	TEMP=TT1-TT2+TT3	
	PTWH=(TEMPH-TEMP)/(HHH-HH)*1.D-7	
	PTWP=(TEMP-TEMP)/(PPP-PP)*1.D-7	
C	STEAM VISCOSITY -	PRP1830
C	1967 ASME STEAM TABLES FORMULA (P. 74) -	PRP1840
	VS=1.0E-06*(.407*TEMP+80.4)	PRP1850
C		PRP1860
C	SPACE -	PRP1870
	XN(I,J)=DS/VS	PRP1880
	TM(I,J)=DS*HH/VS*10.**7	PRP1890
	DTH(I,J)=PTWH	PRP1900
	DTP(I,J)=PTWP	PRP1910
C	TIME -	PRP1920
	C(I,J)=PDWP*PHI(I,J)*HH*10.**7+PHFWT*PTWP*DF*(1.0-PHI(I,J))	PRP1930

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      C(I,J)=C(I,J)+DS*HH*1.07*BETA*PHIO(I,J)-PHIO(I,J)*BETA*DF*PHFWT*TEMP1940
1MP      PRP1950
      D(I,J)=PDWH*PHI(I,J)*HH*10.**7+PHFWT*PHWH*DF*(1.0-PHI(I,J))+DS*PHI1960
1(I,J)      PRP1970
      F(I,J)=PHI(I,J)*PDWP+DS*BETA*PHIO(I,J)      PRP1980
      G(I,J)=PHI(I,J)*PDWH      PRP1990
C      PRP2000
      SW1(I,J)=0.D0      PRP2010
      TEMP2(I,J)=TEMP      PRP2020
      DEN2(I,J)=DS      PRP2030
      QH(I,J)=Q(I,J)*HH*10.**7      PRP2040
60 CONTINUE      PRP2050
      IF (COEF.LT.0.1) GO TO 80      PRP2060
C      PRP2070
C      TRANSIENT CONDUCTIVE HEAT LEAKAGE ONLY -      PRP2080
      IF (KKK.NE.1) GO TO 70      PRP2090
      IC=L+KKK      PRP2100
      II=NP(I,J)      PRP2110
      CALL VERTCD(DELTA,TEMP,COEF,COND,CQQ,II,IC)      PRP2120
C      PRP2130
      CQQ=CQQ*DX(I)*DY(J)      PRP2140
      CQ(I,J)=CQQ      PRP2150
70 CONTINUE      PRP2160
      QH(I,J)=QH(I,J)+CQ(I,J)      PRP2170
80 CONTINUE      PRP2180
      IF (KKK.NE.1) GO TO 120      PRP2190
C      PRINT THERMO DATA EVERY IPRT TIME STEP -      PRP2200
      IF (MOD(L,IPRT).NE.0) GO TO 120      PRP2210
      PRINT 130      PRP2220
      DO 90 J=1,NY      PRP2230
      PRINT 140, (SW1(I,J),I=1,NX)      PRP2240
90 CONTINUE      PRP2250
      PRINT 150      PRP2260
      DO 100 J=1,NY      PRP2270
      PRINT 140, (TEMP2(I,J),I=1,NX)      PRP2280
100 CONTINUE      PRP2290
      PRINT 160      PRP2300
      DO 110 J=1,NY      PRP2310
      PRINT 140, (DEN2(I,J),I=1,NX)      PRP2320
110 CONTINUE      PRP2330
120 CONTINUE      PRP2340
      RETURN      PRP2350
C      PRP2360
130 FORMAT (//11X,'WATER SATURATIONS'/11X,17(1H-)//)      PRP2370
140 FORMAT (/(11X,8(G12.5,2X)))      PRP2380
150 FORMAT (//11X,'TEMPERATURES'/11X,12(1H-)//)      PRP2390
160 FORMAT (//11X,'DENSITY'/11X,7(1H-)//)      PRP2400
      END      PRP2410-

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	SUBROUTINE VERTCD(DEL,TT,COEF,COND,CW,II,IC)	VRT 10
C	*****	VRT 20
	IMPLICIT REAL*8(A-H,O-Z)	VRT 30
C		VRT 40
C	CALLED FROM PRPTY	VRT 50
C	PURPOSE: TO COMPUTE VERTICAL CONDUCTIVE LEAKAGE THROUGH THE	VRT 60
C	CONFINING BED BY THE FINITE ELEMENT METHOD	VRT 70
C	-----	VRT 80
	DIMENSION A(9), B(9), C(9), D(9), F(9), DTEMP(200,11), DELZ(200,10)	VRT 90
	1), TI(200), DDTEMP(200,11)	VRT 100
C	-----	VRT 110
C		VRT 120
C	COMPUTE DELTA Z (ON FIRST TIME STEP) -	VRT 130
	CTHK1=102300.D0	VRT 140
	IF (IC.NE.2) GO TO 30	VRT 150
	NNZ=11	VRT 160
C	NNZ - NUMBER OF NODES IN Z-DIRECTION	VRT 170
C	COMPUTE DELZ (BASED ON TEN ELEMENTS AND DOUBLING THE SIZE OF EACH	VRT 180
C	ELEMENT) -	VRT 190
	NNL=NNZ-1	VRT 200
C	NNL - NUMBER OF ELEMENTS IN Z-DIRECTION	VRT 210
	DELZ(11,NNL)=CTHK1/1023.D0	VRT 220
	SUM=DELZ(11,NNL)	VRT 230
	JSTOP=NNL-2	VRT 240
	DO 10 JJ=1,JSTOP	VRT 250
	DELZ(11,NNL-JJ)=2.*DELZ(11,NNL-JJ+1)	VRT 260
10	SUM=SUM+DELZ(11,NNL-JJ)	VRT 270
	DELZ(11,1)=CTHK1-SUM	VRT 280
C		VRT 290
C	INITIALIZE TI AND DDTEMP -	VRT 300
	TI(11)=TT	VRT 310
	DO 20 J=1,NNZ	VRT 320
20	DDTEMP(11,J)=0.D0	VRT 330
30	CONTINUE	VRT 340
C		VRT 350
C	INITIALIZE DTEMP -	VRT 360
	DO 40 J=1,NNZ	VRT 370
40	DTEMP(11,J)=DDTEMP(11,J)	VRT 380
C		VRT 390
C	FACTOR FOR TIME-DERIVATIVE -	VRT 400
	THETA=1.D0	VRT 410
C		VRT 420
C	SEE COATS,ET.AL., SPE J (DEC 1974) 590 FOR 1-DIM EQUATION.	VRT 430
C	BOUNDARY CONDITIONS -	VRT 440
C	UPPER -	VRT 450
	DTEMP(11,1)=0.D0	VRT 460
C	LOWER -	VRT 470
	DTEMP(11,NNZ)=TT-TI(11)	VRT 480
C		VRT 490
C		VRT 500
C	CALCULATE FINITE ELEMENT COEFFICIENTS FOR MATRIX EQUATION -	VRT 510
	J=0	VRT 520

	DO 50 I=2,NNL	VKT 530
	J=J+1	VKT 540
	A1=DELZ(II,I-1)*COEF/(6.00*DELZ)	VKT 550
	C1=DELZ(II,I)*COEF/(6.00*DELZ)	VKT 560
C		VKT 570
	A(J)=A1-THETA/DELZ(II,I-1)	VKT 580
	B(J)=2.00*A1+THETA/DELZ(II,I-1)+2.00*C1+THETA/DELZ(II,I)	VKT 590
	C(J)=C1-THETA/DELZ(II,I)	VKT 600
C	RIGHT-HAND SIDE -	VKT 610
C	USE DTEMP FROM LAST SOLUTION AS INITIAL CONDITIONS	VKT 620
	D(J)=(A1+(1.00-THETA)/DELZ(II,I-1))*DTEMP(II,I-1)+(2.00*A1-(1.00-	VKT 630
	1THETA)/DELZ(II,I-1)+2.00*C1-(1.00-THETA)/DELZ(II,I))*DTEMP(II,I)+	VKT 640
	2(C1+(1.00-THETA)/DELZ(II,I))*DTEMP(II,I+1)	VKT 650
	50 CONTINUE	VKT 660
C		VKT 670
C	SOLVE BY THOMAS METHOD (SEE CALIF BULL NO 63-4 SEPT, 1971 P 521)	VKT 680
C	NOTE THAT THERE ARE NNZ-2=J EQUATIONS AND J UNKNOWN	VKT 690
C		VKT 700
C	UPPER TRIANGULARIZE -	VKT 710
	F(1)=B(1)	VKT 720
	D(1)=D(1)-A(1)*DTEMP(II,1)	VKT 730
	D(J)=D(J)-C(J)*DTEMP(II,NNZ)	VKT 740
	DO 60 I=2,J	VKT 750
	F(I)=B(I)-C(I-1)*A(I)/F(I-1)	VKT 760
	60 D(I)=D(I)-A(I)*D(1-1)/F(I-1)	VKT 770
C		VKT 780
C	BACK SUBSTITUTE -	VKT 790
	DTEMP(II,J+1)=D(J)/F(J)	VKT 800
	J1=J-1	VKT 810
	DO 70 I=1,J1	VKT 820
	70 DTEMP(II,J+1-I)=(D(J-I)-C(J-I)*DTEMP(II,J+2-I))/F(J-I)	VKT 830
C		VKT 840
C	DTEMP NOW CONTAINS NEW VALUES FOR TEMPERATURE DIFFERENCE	VKT 850
C		VKT 860
C	COMPUTE TRANSIENT CONDUCTIVE LEAKAGE	VKT 870
	CQ=-2.00*COND*(DTEMP(II,NNZ)-DTEMP(II,NNZ-1))/DELZ(II,NNL)	VKT 880
C		VKT 890
C	SAVE DTEMP	VKT 900
	DO 80 J=1,NNZ	VKT 910
	80 DTEMP(II,J)=DTEMP(II,J)	VKT 920
	RETURN	VKT 930
	END	VKT 940-

	SUBROUTINE FORMEQ(A,R,NBBD,MBED)	FEG 10
C	*****	FEG 20
	IMPLICIT REAL*8(A-H,O-Z)	FEG 30
C	CALLED FROM MAIN	FEG 40
C	PURPOSE: TO FORM THE FINAL MATRIX EQUATION	FEG 50
C	-----	FEG 60
	DIMENSION A(NBBD,MBED), R(NBBD)	FEG 70
C		FEG 80
	COMMON /INPUT/ PHI(20,10),XK(20,10),YK(20,10),P(20,10),H(20,10),X(FEG 90	
	1400),X1(400),NP(20,10),NPP(200,2),DX(20),DY(10),DZ(20,10),G(20,10)	FEG 100
	COMMON /CONTROL/ NK,NX,NXX,NY,NYY,NB,NDB,NT,DELT,TIME,PHFWT,DF,XKC,FEG 110	
	1COND,COEF,BETA,IPRT	FEG 120
	COMMON /WORK/ AX(21,10),BX(21,10),EX(21,10),AY(20,11),BY(20,11),EY(FEG 130	
	1(20,11),TX(21,10),TXK(21,10),TY(20,11),TYK(20,11),XM(20,10),XMASS(FEG 140	
	220,10),EN(20,10),ENERGY(20,10),C(20,10),D(20,10),F(20,10),G(20,10)	FEG 150
	3,QH(20,10),XN(20,10),IM(20,10),DTP(20,10),DTH(20,10),PHIC(20,10),PFEG 160	
	4OLD(20,10)	FEG 170
	COMMON /EXTRA/ MBW,MBL	FEG 180
C	-----	FEG 190
	MP=(MBW+1)/2	FEG 200
C	MP = MAIN DIAGONAL (STORED VERTICALLY)	FEG 210
C		FEG 220
C	INITIALIZE ARRAYS -	FEG 230
	DO 10 K=1,NBB	FEG 240
	DO 10 KK=1,MBW	FEG 250
10	A(K,KK)=0.00	FEG 260
C		FEG 270
C	COMPUTE MATRIX -	FEG 280
	DO 50 K=1,NB	FEG 290
	I=NPP(K,1)	FEG 300
	J=NPP(K,2)	FEG 310
C		FEG 320
C	MAIN DIAGONAL TERMS -	FEG 330
C	PRESSURE -	FEG 340
	A(2*K-1,MP)=-EX(I,J)-EY(I,J)-EX(I+1,J)-EY(I,J+1)	FEG 350
C	ENTHALPY -	FEG 360
	A(2*K,MP-1)=-AX(I,J)-AY(I,J)-AX(I+1,J)-AY(I,J+1)	FEG 370
	A(2*K,MP)=-BX(I,J)-BY(I,J)-BX(I+1,J)-BY(I,J+1)	FEG 380
C		FEG 390
C	OFF DIAGONAL TERMS -	FEG 400
	II=I	FEG 410
	IF (J.EQ.1) GO TO 20	FEG 420
	JJ=J-1	FEG 430
	NN=NP(II,JJ)	FEG 440
	IF (NN.EQ.0) GO TO 20	FEG 450
	NC=MP+(NN-K)*2	FEG 460
	A(2*K-1,NC)=EY(I,J)	FEG 470
	A(2*K,NC-1)=AY(I,J)	FEG 480
	A(2*K,NC)=BY(I,J)	FEG 490
20	CONTINUE	FEG 500
	IF (J.EQ.NY) GO TO 30	FEG 510
	JJ=J+1	FEG 520

NN=NP(II,JJ)	FEG 530
IF (NN.EQ.0) GO TO 30	FEG 540
NC=MP+(NN-K)*2	FEG 550
A(2*K-1,NC)=EY(I,J+1)	FEG 560
A(2*K,NC-1)=AY(I,J+1)	FEG 570
A(2*K,NC)=BY(I,J+1)	FEG 580
30 JJ=J	FEG 590
IF (I.EQ.1) GO TO 40	FEG 600
II=I-1	FEG 610
NN=NP(II,JJ)	FEG 620
IF (NN.EQ.0) GO TO 40	FEG 630
NC=MP+(NN-K)*2	FEG 640
A(2*K-1,NC)=EX(I,J)	FEG 650
A(2*K,NC-1)=AX(I,J)	FEG 660
A(2*K,NC)=BX(I,J)	FEG 670
40 IF (I.EQ.NX) GO TO 50	FEG 680
II=I+1	FEG 690
NN=NP(II,JJ)	FEG 700
IF (NN.EQ.0) GO TO 50	FEG 710
NC=MP+(NN-K)*2	FEG 720
A(2*K-1,NC)=EX(I+1,J)	FEG 730
A(2*K,NC-1)=AX(I+1,J)	FEG 740
A(2*K,NC)=BX(I+1,J)	FEG 750
50 CONTINUE	FEG 760
C	FEG 770
C COMPUTE KNOWN VECTOR -	FEG 780
DO 70 K=1,NBB	FEG 790
II=K-MP	FEG 800
R(K)=0.00	FEG 810
DO 60 JJ=1,MBW	FEG 820
II=II+1	FEG 830
IF (II.LT.1) GO TO 60	FEG 840
IF (II.GT.NBB) GO TO 70	FEG 850
R(K)=R(K)+A(K,JJ)*X1(II)	FEG 860
60 CONTINUE	FEG 870
70 CONTINUE	FEG 880
C	FEG 890
DO 80 K=1,NB	FEG 900
I=NPP(K,1)	FEG 910
J=NPP(K,2)	FEG 920
C	FEG 930
C NEWTON-RAPHSON RESIDUAL VECTOR -	FEG 940
R(2*K-1)=-R(2*K-1)+XM(I,J)/DELT-XMASS(I,J)/DELT-G(I,J)	FEG 950
R(2*K)=-R(2*K)+EN(I,J)/DELT-ENERGY(I,J)/DELT-QH(I,J)	FEG 960
C	FEG 970
C LINEARIZED NEWTON-RAPHSON MATRIX -	FEG 980
A(2*K-1,MP)=A(2*K-1,MP)-F(I,J)*DX(I)*DZ(I,J)*DY(J)/DELT	FEG 990
A(2*K-1,MP+1)=A(2*K-1,MP+1)-G(I,J)*DX(I)*DY(J)*DZ(I,J)/DELT	FEG 1000
A(2*K,MP-1)=A(2*K,MP-1)-C(I,J)*DX(I)*DY(J)*DZ(I,J)/DELT	FEG 1010
A(2*K,MP)=A(2*K,MP)-D(I,J)*DX(I)*DY(J)*DZ(I,J)/DELT	FEG 1020
80 CONTINUE	FEG 1030
RETURN	FEG 1040
END	FEG 1050-

	SUBROUTINE SOLVE(KKK,B,R,NEQ,IHALFB,NDIM,MDIM)	SOL 10
C	*****	SOL 20
	IMPLICIT REAL*8(A-H,O-Z)	SOL 30
C		SOL 40
C	ASYMMETRIC BAND MATRIX EQUATION SOLVER	SOL 50
C	ORIGINALLY PROGRAMED BY JAMES C. DUGUID	SOL 60
C		SOL 70
C	KKK=1 TRIANGULARIZES THE BAND MATRIX B	SOL 80
C	KKK=2 SOLVES FOR RIGHT SIDE R, SOLUTION RETURNS IN R	SOL 90
C		SOL 100
	DIMENSION B(NDIM,MDIM), R(MDIM)	SOL 110
	NRS=NEQ-1	SOL 120
	IHBP=IHALFB+1	SOL 130
	IF (KKK.EQ.2) GO TO 30	SOL 140
C		SOL 150
C	TRIANGULARIZE MATRIX A USING DOOLITTLE METHOD	SOL 160
C		SOL 170
	DO 20 K=1,NRS	SOL 180
	PIVOT=B(K,IHBP)	SOL 190
	KK=K+1	SOL 200
	KC=IHBP	SOL 210
	DO 10 I=KK,NEQ	SOL 220
	KC=KC-1	SOL 230
	IF (KC.LE.0) GO TO 20	SOL 240
	C=-B(1,KC)/PIVOT	SOL 250
	B(1,KC)=C	SOL 260
	KI=KC+1	SOL 270
	LIM=KC+IHALFB	SOL 280
	DO 10 J=KI,LIM	SOL 290
	JC=IHBP+J-KC	SOL 300
10	B(I,J)=B(1,J)+C*B(K,JC)	SOL 310
20	CONTINUE	SOL 320
	GO TO 100	SOL 330
C		SOL 340
C	MODIFY LOAD VECTOR R	SOL 350
C		SOL 360
30	NN=NEQ+1	SOL 370
	IBAND=2*IHALFB+1	SOL 380
	DO 70 I=2,NEQ	SOL 390
	JC=IHBP-I+1	SOL 400
	J1=1	SOL 410
	IF (JC.LE.0) GO TO 40	SOL 420
	GO TO 50	SOL 430
40	JC=1	SOL 440
	J1=I-IHBP+1	SOL 450
50	SUM=0.0	SOL 460
	DO 60 J=JC,IHALFB	SOL 470
	SUM=SUM+B(I,J)*R(J1)	SOL 480
60	J1=J1+1	SOL 490
70	R(I)=R(I)+SUM	SOL 500
C		SOL 510
C	BACK SOLUTION	SOL 520

C

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R(NEQ)=R(NEW)/B(NEW,IHBP)
DO 90 IBACK=2,NEQ
I=NN-IBACK
JP=I
KR=IHBP+1
MR=MIN0(IBAND,IHALFB+IBACK)
SUM=0.0
DO 80 J=KR,MR
JP=JP+1
80 SUM=SUM+B(I,J)*R(JP)
90 R(I)=(R(I)-SUM)/B(I,IHBP)
100 RETURN
END

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SOL 530
SOL 540
SOL 550
SOL 560
SOL 570
SOL 580
SOL 590
SOL 600
SOL 610
SOL 620
SOL 630
SOL 640
SOL 650
SOL 660-

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	SUBROUTINE PDATA(P,H,TIME,L,NY,NX)	PDT 10
C	*****	PDT 20
	IMPLICIT REAL*8(A-H,O-Z)	PDT 30
C		PDT 40
C	CALLED FROM MAIN	PDT 50
C	PURPOSE: TO PRINT COMPUTED PRESSURE AND ENTHALPY	PDT 60
C	-----	PDT 70
	DIMENSION P(20,10), H(20,10)	PDT 80
C	-----	PDT 90
C		PDT 100
	PRINT 30, L, TIME	PDT 110
	DO 10 J=1, NY	PDT 120
10	PRINT 40, (P(I,J), I=1, NX)	PDT 130
	PRINT 50	PDT 140
	DO 20 J=1, NY	PDT 150
20	PRINT 40, (H(I,J), I=1, NX)	PDT 160
	RETURN	PDT 170
C		PDT 180
	30 FORMAT (///11X, 'STEP NUMBER', I4, 10X, 'TIME', E10.3/11X, 15(1H*)///11XPDT 190	
	1, 'PRESSURE VALUES'/11X, 15(1H-)//)	PDT 200
	40 FORMAT (/(11X, 8(G12.5, 2X)))	PDT 210
	50 FORMAT (///11X, 'ENTHALPY VALUES'/11X, 15(1H-)//)	PDT 220
	END	PDT 230-

	SUBROUTINE PHREG(INDEX)	PHR 05
C	*****	PHR 10
	IMPLICIT REAL*8(A-H,O-Z)	PHR 20
C		PHR 25
C	CALLED FROM MAIN	PHR 30
C	PURPOSE: TO DETERMINE WHAT THERMODYNAMIC REGION A	PHR 40
C	FINITE-DIFFERENCE BLOCK IS IN	PHR 50
C	-----	PHR 60
	DIMENSION INDEX(200)	PHR 70
C		PHR 80
	COMMON /INPUT/ PHI(20,10),XK(20,10),YK(20,10),P(20,10),H(20,10),X(PHR 90
	1400),X1(400),NP(20,10),NPP(200,2),DX(20),DY(10),DZ(20,10),Q(20,10)	PHR 100
	COMMON /CONTRO/ NK,NX,NXX,NY,NYY,NB,NBB,NT,DELT,TIME,PHFWT,DF,XKC,PHR	PHR 110
	1COND,COEF,BETA,IPRT	PHR 120
C	-----	PHR 130
C	INDEX=-1 FOR COMPRESSED WATER	PHR 140
C	INDEX=0 FOR TWO-PHASE	PHR 150
C	INDEX=1 FOR SUPERHEATED STEAM	PHR 160
	DO 10 K=1,NB	PHR 170
	PP=X1(2*K-1)*0.1**7	PHR 180
	HH=X1(2*K)*0.1**7	PHR 190
C	COMPUTE SATURATED STEAM (HS) AND SATURATED WATER (HW) ENTHALPY -	PHR 200
	HS=2822.82-39.952/PP+2.54342/PP/PP-0.938879*PP*PP	PHR 210
	HW=730.984+129.239*PP-10.0333*PP*PP+0.39881*PP*PP*PP	
1	-99.0697/PP+12.9267/PP/PP-0.628359/PP/PP/PP	
	INDEX(K)=0	PHR 240
	IF (HH.LT.HW) INDEX(K)=-1	PHR 250
	IF (HH.GT.HS) INDEX(K)=1	PHR 260
C	IF TEMPERATURE IS BELOW 50 DEG C (H=209.33) ASSUME IN COMP WATER	PHR 270
	IF (HH.LT.209.33D0) INDEX(K)=-1	PHR 280
10	CONTINUE	PHR 290
	RETURN	PHR 300
	END	PHR 310-

	SUBROUTINE BALNCE(ICX,KKK,PCEE)	BAL 05
C	*****	BAL 10
	IMPLICIT REAL*8(A-H,O-Z)	BAL 20
C		BAL 30
C	CALLED FROM MAIN	BAL 40
C	PURPOSE: TO COMPUTE MASS AND ENERGY BALANCE	BAL 50
C	-----	BAL 60
	COMMON /INPUT/ PHI(20,10),XK(20,10),YK(20,10),P(20,10),H(20,10),X(BAL 70
	1400),X1(400),NP(20,10),NPP(200,2),DX(20),DY(10),DZ(20,10),Q(20,10)	BAL 80
	COMMON /CONTRO/ NK,NX,NXX,NY,NYY,NB,NBB,NT,DELT,TIME,PHFWT,DF,XKC,	BAL 90
	1COND,COEF,BETA,IPRT	BAL 100
	COMMON /WORK/ AX(21,10),BX(21,10),EX(21,10),AY(20,11),BY(20,11),EY	BAL 110
	1(20,11),TX(21,10),TXK(21,10),TY(20,11),TYK(20,11),XM(20,10),XMASS(BAL 120
	220,10),EN(20,10),ENERGY(20,10),C(20,10),D(20,10),F(20,10),G(20,10)	BAL 130
	3,QH(20,10),XN(20,10),TM(20,10),DTP(20,10),DTH(20,10),PHIO(20,10),P	BAL 140
	4OLD(20,10)	BAL 150
	COMMON /CHECK/ IND(200),INDOLD(200)	BAL 160
C	-----	BAL 170
C		BAL 180
C	STATEMENT FUNCTIONS FOR THERMODYNAMIC PROPERTIES -	BAL 190
C		BAL 200
	F1(PX,HX)=1.00207+4.42607D-4*PX-5.47456D-5*HX+5.02875D-7*HX*PX-1.2	BAL 210
	14791D-7*HX*HX	BAL 220
	F2(PX,HX)=-2.41231+2.56222D-1*HX-9.31415D-3*PX*PX-2.2568D-5*HX*HX	BAL 230
	F3(PX,HX)=-2.26162D-5+0.0438441D0*PX-1.79088D-5*PX*HX+3.69276D-8*P	BAL 240
	1X*PX*PX*PX+5.17644D-13*HX*HX*HX*PX	BAL 250
	F4(PX,HX)=-374.669D0+47.9921D0*PX-0.633606D0*PX*PX+7.39386D-5*HX*H	BAL 260
	1X-3.3372D6/HX/HX/PX/PX+0.0357154D0/PX/PX/PX-1.1725D-9*HX*HX*HX*PX	BAL 270
	22.26861D15/HX/HX/HX/HX	BAL 280
C		BAL 290
	DELM=0.D0	BAL 300
	DELE=0.D0	BAL 310
	DO 70 I=1,NX	BAL 320
	DO 70 J=1,NY	BAL 330
	IF (DZ(I,J).GT.0.D0) GO TO 10	BAL 340
	XM(I,J)=0.D0	BAL 350
	EN(I,J)=0.D0	BAL 360
	GO TO 70	BAL 370
10	CONTINUE	BAL 380
	PP=P(I,J)	BAL 390
	HH=H(I,J)	BAL 400
	PP=PP*0.1**7	BAL 410
	HH=HH*0.1**7	BAL 420
	K=NP(I,J)	BAL 430
	PHI(I,J)=PHIO(I,J)*(1.D0+(P(I,J)-POLD(I,J))*BETA)	BAL 440
	HW=730.984+129.239*PP-10.0333*PP*PP+0.39881*PP*PP*PP	
1	-99.0697/PP+12.9267/PP/PP-0.628359/PP/PP/PP	
	IF (IND(K)) 20,30,40	BAL 470
20	CONTINUE	BAL 480
	DEN=F1(PP,HH)	BAL 490
	TEMP=F2(PP,HH)	BAL 500
	GO TO 50	BAL 510

30	CONTINUE	BAL 520
	HS=2822.82-39.952/PP+2.54342/PP/PP-0.938879*PP*PP	BAL 530
	TEMP=F2(PP,HW)	BAL 540
	DW=F1(PP,HW)	BAL 550
	DS=F3(PP,HS)	BAL 560
	SW=DS*(HS-HH)/(HH*(DW-US)-(HW*DW-HS*DS))	BAL 570
	SST=1.0-SW	BAL 580
	DEN=DW*SW+SST*DS	BAL 590
	GO TO 50	BAL 600
40	CONTINUE	BAL 610
	DEN=F3(PP,HH)	BAL 620
	HW=730.984+129.239*PP-10.0333*PP*PP+0.39881*PP*PP*PP	
1	-99.0697/PP+12.9267/PP/PP-0.628359/PP/PP/PP	
	HS=2822.82-39.952/PP+2.54342/PP/PP-0.938879*PP*PP	
	TT1=F4(PP,HH)	
	TT2=F4(PP,HS)	
	TT3=F2(PP,HW)	
	TEMP=TT1-TT2+TT3	
50	HROCK=TEMP*PHFWT	BAL 640
	VOL*DY(J)*DX(I)*DZ(I,J)	BAL 650
	XMT=VOL*DEN*PHI(I,J)	BAL 660
	ENT=VOL*(PHI(I,J)*HH*DEN*10.**7+(1.0-PHI(I,J))*HROCK*DF)	BAL 670
	IF (ICX.EQ.0) GO TO 60	BAL 680
	DELM=DELM-XMASS(I,J)*XMT	BAL 690
	DELE=DELE-ENERGY(I,J)*ENT	BAL 700
60	XM(I,J)=XMT	BAL 710
	EN(I,J)=ENT	BAL 720
70	CONTINUE	BAL 730
	IF (KKK.NE.NK) GO TO 90	BAL 740
	DO 80 I=1,NX	BAL 750
	DO 80 J=1,NY	BAL 760
	XMASS(I,J)=XM(I,J)	BAL 770
80	ENERGY(I,J)=EN(I,J)	BAL 780
90	CONTINUE	BAL 790
	IF (ICX.EQ.0) GO TO 110	BAL 800
	QQQ=0.D0	BAL 810
	EEE=0.D0	BAL 820
	DO 100 I=1,NX	BAL 830
	DO 100 J=1,NY	BAL 840
	QQQ=QQQ+Q(I,J)*DELT	BAL 850
100	EEE=EEE+QH(I,J)*DELT	BAL 860
	PCEM=(DELM-QQQ)*100.D0	BAL 870
	IF (QQQ.NE.0.D0) PCEM=PCEM/QQQ	BAL 880
	PCEE=(DELE-EEE)*100.D0	BAL 890
	IF (EEE.NE.0.D0) PCEE=PCEE/EEE	BAL 900
	WRITE (6,120) QQQ,EEE,DELM,DELE,PCEM,PCEE	BAL 910
110	CONTINUE	BAL 920
	RETURN	BAL 930
		BAL 940
C		
120	FORMAT (//11X,23HMASS AND ENERGY BALANCE/11X,23(1H-)/32X,4HMASS,31BAL 950	
	1X,4HHEAT/15X,12HDISCHARGE - ,G15.8,20X,G15.8/15X,12HSTORAGE - ,GBAL 960	
	215.8,20X,G15.8/15X,12H* ERROR - ,G15.8,20X,G15.8)	BAL 970
	END	BAL 980-